

1            **pyUserCalc: A revised Jupyter notebook calculator for**  
2            **uranium-series disequilibria in basalts**

3            **Lynne J. Elkins<sup>1</sup>, Marc Spiegelman<sup>2</sup>**

4            <sup>1</sup>University of Nebraska-Lincoln, Lincoln, NE, USA, lelkins@unl.edu

5            <sup>2</sup>Lamont-Doherty Earth Observatory of Columbia University, Palisades, NY, USA, mspieg@ldeo.columbia.edu

6            **Key Points:**

- 7            • Cloud-based Jupyter notebook presents an open source, reproducible tool  
8            for modeling U-series in basalts
- 9            • Equilibrium and pure disequilibrium porous flow U-series models with 1D  
10           conservation of mass
- 11           • Scaled porous flow model introduces incomplete equilibrium scenario with  
12           reaction rate limitations

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Corresponding author: Lynne J. Elkins, lelkins@unl.edu

## Abstract

Meaningful analysis of uranium-series isotopic disequilibria in basaltic lavas relies on the use of complex forward numerical models like dynamic melting (McKenzie, 1985) and equilibrium porous flow (Spiegelman and Elliott, 1993). Historically, such models have either been solved analytically for simplified scenarios, such as constant melting rate or constant solid/melt trace element partitioning throughout the melting process, or have relied on incremental or numerical calculators with limited power to solve problems and/or restricted availability. The most public numerical solution to reactive porous flow, UserCalc (Spiegelman, 2000) was maintained on a private institutional server for nearly two decades, but that approach has been unsustainable in light of modern security concerns. Here we present a more long-lasting solution to the problems of availability, model sophistication and flexibility, and long-term access in the form of a cloud-hosted, publicly available Jupyter notebook. Similar to UserCalc, the new notebook calculates U-series disequilibria during time-dependent, equilibrium partial melting in a one-dimensional porous flow regime where mass is conserved. In addition, we also provide a new disequilibrium transport model which has the same melt transport model as UserCalc, but approximates rate-limited diffusive exchange of nuclides between solid and melt using linear kinetics. The degree of disequilibrium during transport is controlled by a Damköhler number, allowing the full spectrum of equilibration models from complete fractional melting ( $Da = 0$ ) to equilibrium transport ( $Da = \infty$ ).

## 1 Introduction

Continuous forward melting models are necessary to interpret the origins of empirically-measured U-series isotopic disequilibria in basaltic lavas, but the limited and unreliable availability of reproducible tools for making such calculations remains a persistent problem for geochemists. To date, a number of models have been developed for this task, including classical dynamic melting after McKenzie (1985) and the reactive porous flow model of Spiegelman and Elliott (1993). There have since been numerous approaches to using both the dynamic and porous flow models that range from simplified analytical solutions (e.g., Sims et al., 1999; Zou, 1998; Zou and Zindler, 2000) to incremental dynamic melting calculators (Stracke et al., 2003), two-porosity calculators (Jull et al., 2002; Lundstrom et al., 2000; Sims et al., 2002), and one-dimensional numerical solutions to reactive porous flow (Spiegelman, 2000) and dynamic melting (Bourdon et al., 2005; Elkins et al., 2019). Unfortunately, some of the approaches published since 1990 lacked publicly available tools that would permit others to directly apply the authors' methods, and while the more simplified and incremental approaches remain appropriate for asking and approaching some questions, they are insufficient for other applications that require more complex approaches (e.g., two-lithology melting; Elkins et al., 2019). Other tools like UserCalc that were available to public users (Spiegelman, 2000) were limited in application and have since become unavailable.

In light of the need for more broadly accessible and flexible solutions to U-series disequilibrium problems in partial melting, here we present a cloud-server hosted, publicly available numerical calculator for one-dimensional, decompression partial melting. The tool is provided in a Jupyter notebook with importable Python code and can be accessed from a web browser. Users will be able to access and use the tool using a free cloud server account, or on their own computer given any standard Python distribution. As shown below, the notebook is structured to permit the user to select one of two primary model versions, either classical reactive porous flow after Spiegelman and Elliott (1993) and Spiegelman (2000),

65 or a new disequilibrium transport model, developed after the appendix formulas  
 66 of Spiegelman and Elliott (1993). The new model ranges from pure disequilibrium  
 67 porous flow transport (i.e., the mass-conserved equivalent of true fractional melt-  
 68 ing over time) to a "scaled" disequilibrium scenario, where the degree of chemical  
 69 equilibrium that is reached is determined by the relationship between the rate of  
 70 chemical reaction and the solid decompression rate (which is, in turn, related to  
 71 the overall melting rate), in the form of a Damköhler number.

72 This scaled disequilibrium model resembles the classic dynamic melting model of  
 73 McKenzie (1985), with the caveat that ours is the first U-series melting model de-  
 74 veloped for near-fractional, disequilibrium transport where mass is also conserved  
 75 within a one-dimensional melting regime. That is, rather than controlling the  
 76 quantity of melt that remains in equilibrium with the solid using a fixed residual  
 77 porosity, the melt porosity is controlled by Darcy's Law and mass conservation  
 78 constraints after Spiegelman and Elliott (1993), and the "near-fractional" scenario  
 79 is simulated using the reaction rate of the migrating liquid with the upwelling  
 80 solid matrix.

## 81 **2 Calculating U-series in basalts during mass-conserved, one-dimensional** 82 **porous flow**

### 83 **2.1 Solving for equilibrium transport**

84 Here we consider several forward melting models that calculate the concen-  
 85 trations and activities of U-series isotopes ( $^{238}\text{U}$ ,  $^{230}\text{Th}$ ,  $^{226}\text{Ra}$ ,  $^{235}\text{U}$ , and  $^{231}\text{Pa}$ )  
 86 during partial melting and melt transport due to adiabatic mantle decompression.  
 87 Following Spiegelman and Elliott (1993), we start with conservation of mass equa-  
 88 tions for the concentration of a nuclide  $i$ , assuming chemical equilibrium between  
 89 melt and solid:

$$90 \quad \frac{\partial}{\partial t} [\rho_f \phi + \rho_s (1 - \phi) D_i] c_i^f + \nabla \cdot [\rho_f \phi v + \rho_s (1 - \phi) D_i V] c_i^f = \lambda_{i-1} [\rho_f \phi + \rho_s (1 - \phi) D_{i-1}] c_{i-1}^f - \lambda_i [\rho_f \phi + \rho_s (1 - \phi) D_i] c_i^f \quad (1)$$

91 where  $t$  is time,  $c_i^f$  is the concentration of nuclide  $i$  in the melt,  $D_i$  is the bulk  
 92 solid/liquid partition coefficient for nuclide  $i$ ,  $\rho_f$  is the density of the fluid and  
 93  $\rho_s$  is the density of the solid,  $\phi$  is the porosity (local volume fraction of melt),  $v$  is  
 94 the velocity of the melt and  $V$  the velocity of the solid in three dimensions,  $\lambda_i$  is  
 95 the decay constant of nuclide  $i$ , and  $(i - 1)$  indicates the radioactive parent of nu-  
 96 clide  $i$  see Table 1. Equation (1) states that the change in total mass of nuclide  $i$  in  
 97 both the melt and the solid is controlled by the divergence of the mass flux trans-  
 98 ported by both phases and by the radioactive decay of both parent and daughter  
 99 nuclides (i.e., the right hand side of the equation above).

Table 1: List of Variables Used in This Study

Variable	Definition
$c_i^f$	Concentration of nuclide $i$ in the liquid
$c_i^s$	Concentration of nuclide $i$ in the solid
$U_i^f$	Natural log of the concentration of nuclide $i$ in the liquid relative to its initial concentration
$U_i^s$	Natural log of the concentration of nuclide $i$ in the solid relative to its initial concentration
$U_i^{stable}$	Stable element component of $U_i^f$
$U_i^{rad}$	Radiogenic component of $U_i^f$
$a_i$	Activity of nuclide $i$
$a_i^0$	Initial activity of nuclide $i$
$z$	Height in a one-dimensional melting column
$h$	Total height of the melting column
$\zeta$	$= z/h$ , Dimensionless fractional height in scaled one-dimensional melting column
$D_i$	Bulk solid/liquid partition coefficient for nuclide $i$
$D_i^0$	Initial bulk solid/liquid partition coefficient for nuclide $i$
$\rho_f$	Density of the liquid
$\rho_s$	Density of the solid
$\phi$	Porosity (volume fraction of liquid present)
$\phi_0$	Maximum or reference porosity
$V$	Solid velocity
$v$	Liquid velocity
$W$	One-dimensional solid velocity
$w$	One-dimensional liquid velocity
$W_0$	Solid mantle upwelling velocity
$\lambda_i$	Decay constant for nuclide $i$
$\lambda_i'$	$= \lambda_i h / W_0$ , Decay constant for nuclide $i$ scaled by solid transport time
$\Gamma$	Melting rate
$\Gamma_0$	Constant melting rate
$F_{max}$	Maximum degree of melting
$w_{eff}^i$	Effective liquid velocity of nuclide $i$
$R_i^{i-1}$	Ingrowth factor
$\alpha_i$	Initial degree of secular disequilibrium in the unmelted solid
$k$	Permeability
$K_r$	Relative permeability factor
$n$	Permeability exponent
$A_d$	Permeability calibration function
$\Re$	Reactivity rate factor
$d$	Diffusion/Reaction length scale (e.g., grain-size)
$Da$	Dahmköhler number

100 The equilibrium model of Spiegelman and Elliott (1993) assumes that complete  
101 chemical equilibrium is maintained between the migrating partial melt and the  
102 solid rock matrix along a decompressing one-dimensional column. To close the  
103 equations, they assume that melt transport is described by a simplified form of  
104 Darcy's Law for permeable flow through the solid matrix. In one dimension, for  
105 a steady-state upwelling column of melting mantle rocks, they defined the one-  
106 dimensional melt and solid velocities ( $w$  and  $W$ , respectively), and expressed the  
107 melt and solid fluxes as functions of height ( $z$ ) in terms of a constant melting rate  
108  $\Gamma_0$ :

$$\rho_f \phi w = \Gamma_0 z \quad (2)$$

$$\rho_s(1 - \phi)W = \rho_s W_0 - \Gamma_0 z \quad (3)$$

where  $W_0$  is the solid mantle upwelling rate, and  $\Gamma_0$  is equivalent to  $\rho_s W_0 F_{max}$  divided by the depth  $h$  for a maximum degree of melting  $F_{max}$ .

Assuming an initial condition of secular equilibrium, where the initial activities  $\lambda_i c_{i,0}^f D_i$  are equivalent for parent and daughter nuclides, they derived a system of differential equations for the concentration  $c_i^f$  in any decay chain, which can be solved numerically using equation (10) from that paper:

$$\frac{dc_i^f}{d\zeta} = c_i^f \frac{(D_i - 1)F_{max}}{D_i + (1 - D_i)F_{max}\zeta} + \lambda_i h \left[ \frac{D_i[D_{i-1} + (1 - D_{i-1})F_{max}\zeta]}{D_{i-1}[D_i + (1 - D_i)F_{max}\zeta]} \frac{c_{i-1}^f}{w_{eff}^{i-1}} - \frac{c_i^f}{w_{eff}^i} \right] \quad (4)$$

where  $c_i^f$  is the scaled melt concentration ( $= c_i^f / c_{i,0}^f$ ),  $\zeta$  is the dimensionless fractional height in the scaled column, equal to 0 at the base and 1 at the top, and

$$w_{eff}^i = \frac{\rho_f \phi w + \rho_s(1 - \phi)D_i W}{\rho_f \phi + \rho_s(1 - \phi)D_i} \quad (5)$$

is the effective velocity for element  $i$ .

In their appendix, Spiegelman and Elliott (1993) developed the more general (and, arguably, realistic) form where  $\Gamma$  and  $D_i$  are functions of height  $z$ . The UserCalc model of Spiegelman (2000) then formulated a one-dimensional numerical integration for the concentrations of selected U-series isotopes in continuously produced partial melts with height  $z$ , after the equilibrium formulas above. The concentration expression derived by Spiegelman (2000) for the equilibrium scenario (formula 6 in that reference) is:

$$\frac{dc_i^f}{dz} = \frac{-c_i^f(z)}{F(z) + (1 - F(z))D_i(z)} \frac{d}{dz} [F(z) + (1 - F(z))D_i(z)] + \frac{\lambda_{i-1} \overline{\rho D_{i-1}} c_{i-1}^f(z) - \lambda_i \overline{\rho D_i} c_i^f(z)}{\rho_s W_0 [F(z) + (1 - F(z))D_i(z)]} \quad (6)$$

where  $F$  is the degree of melting. Spiegelman (2000) further observed that solving for the natural log of the concentrations normalized to the initial concentration of  $i$ ,  $U_i$ , rather than the concentrations themselves, is more accurate, particularly for highly incompatible elements (formulas 7-9 in that reference). This is because log concentrations change linearly during melting, rather than exponentially, and are more numerically stable to calculate.

$$U_i^f = \ln \left( \frac{c_i^f}{c_{i,0}^f} \right) \quad (7)$$

$$\frac{dU_i^f}{dz} = \frac{1}{c_i^f(z)} \frac{dc_i^f}{dz} \quad (8)$$

$$\frac{dU_i^f}{dz} = \frac{-1}{F(z) + (1 - F(z))D_i(z)} \frac{d}{dz} [F(z) + (1 - F(z))D_i(z)] + \frac{\lambda_i}{w_{eff}^i} [R_i^{i-1} \exp[U_{i-1}^f(z) - U_i^f(z)] - 1] \quad (9)$$

138

139 For the formulas above, Spiegelman (2000) defined a series of variables that allow  
140 for simpler integration formulas and aid in efficient solution of the model, namely

$$\overline{\rho D_i} = \rho_f \phi + \rho_s (1 - \phi) D_i(z), \quad (10)$$

141

$$\overline{F} = F(z) + (1 - F(z))D_i(z), \quad (11)$$

142

$$R_i^{i-1} = \alpha_i \frac{D_i^0}{D_{i-1}^0} \frac{\overline{\rho D_{i-1}}}{\overline{\rho D_i}}, \quad (12)$$

143

$$\alpha_i = \frac{\lambda_{i-1} c_{(i-1),0}^s}{\lambda_i c_{i,0}^s}, \quad (13)$$

144

145 and substituting from the formulas above

$$w_{eff}^i = \frac{\rho_s W_0 \overline{F}}{\overline{\rho D_i}}. \quad (14)$$

146

147 where  $D_i^0$  is the initial bulk solid/melt partition coefficient for element  $i$ ,  $R_i^{i-1}$  is  
148 the ingrowth factor, and  $\alpha$  is the initial degree of secular disequilibrium in the  
149 unmelted solid.

150  $U_i(z) = \ln(c_f(z)/c_f^0)$ , the log of the total concentration of nuclide  $i$  in the melt,  
151 can then be decomposed into

$$U_i(z) = U_i^{stable}(z) + U_i^{rad}(z) \quad (15)$$

152

153 where

$$U_i^{stable}(z) = \ln \left[ \frac{D_i^0}{\overline{F} D_i(z)} \right] \quad (16)$$

154

155 is the log concentration of a stable nuclide with the same partition coefficients,  
156 and  $U_i^{rad}(z)$  is the radiogenic ingrowth component. An alternate way of writing  
157 the radiogenic ingrowth component of equation (9) of Spiegelman (2000) is:

$$\frac{dU_i^{rad}}{d\zeta} = \lambda_i' \frac{\overline{\rho D_i}}{\overline{F} D_i} \left[ R_i^{i-1} \exp[U_{i-1}(\zeta) - U_i(\zeta)] - 1 \right] \quad (17)$$

158

159 where

$$\lambda'_i = \frac{h\lambda_i}{W_0} \quad (18)$$

is the decay constant of nuclide  $i$ , scaled by the solid transport time ( $h/W_0$ ) across a layer of total height  $h$ . Note Eq. (17) is solved over a column of dimensionless height 1 where  $\zeta \in [0, 1]$ .

Using these equations, the UserCalc reactive porous flow calculator accepted user inputs for both  $F(z)$  and  $D_i(z)$ . The method uses a formula for the melt porosity ( $\phi(z)$ ) based on a Darcy's Law expression with a scaled permeability factor (formula 20 from Spiegelman (2000)):

$$K_r(z)A_d\phi^n(1-\phi)^2 + \phi[1 + F(z)(\frac{\rho_s}{\rho_f} - 1)] - \frac{\rho_s}{\rho_f}F(z) = 0 \quad (19)$$

where  $K_r(z)$  is the scaled permeability with height  $z$ ,  $A_d$  is a permeability calibration function, and  $n$  is the permeability exponent. The permeability exponent for a tube-shaped fluid network is expected to be  $n = 2$ , while for a sheet-shaped network it is 3; recent measurements of the permeabilities of experimental magmatic melt networks suggest realistic magma migration occurs in a manner intermediate between these two scenarios, with  $n = 2.6$  (Miller et al., 2014). The relative permeability  $K_r$  is calculated with respect to the permeability at the top of the column, i.e. depth  $z = z_{final}$ :

$$K_r(z) = \frac{k(z)}{k(z_{final})} \quad (20)$$

and allows for locally enhanced flow (e.g., mimicking the effects of a relatively low viscosity fluid).

Our model implementation reproduces and builds on the prior efforts summarized above, using a readily accessible computer language (Python) and web application (Jupyter notebooks).

## 2.2 Solving for complete disequilibrium transport

We further present a calculation tool that solves a similar set of equations for pure chemical disequilibrium transport during one-dimensional decompression melting. This model assumes that the solid produces an instantaneous fractional melt in local equilibrium with the solid; however, the melt is not allowed to back-react with the solid during transport, as it would in the equilibrium model above. In the limiting condition defined by stable trace elements (i.e., without radioactive decay), the model reduces to the calculation for an accumulated fractional melt. The model solves for the concentration of each nuclide  $i$  in the solid ( $s$ ) and liquid ( $f$ ) using equations (26) and (27) of Spiegelman and Elliott (1993):

$$\frac{dc_i^s}{dz} = \frac{c_i^s(z)(1 - \frac{1}{D_i(z)})}{1 - F(z)} \frac{dF}{dz} + \frac{1 - \phi}{W_0(1 - F(z))} [\lambda_{i-1}c_{i-1}^s(z) - \lambda_i c_i^s(z)] \quad (21)$$

$$\frac{dc_i^f}{dz} = \frac{\frac{c_i^s(z)}{D_i(z)} - c_i^f(z)}{F(z)} \frac{dF}{dz} + \frac{\rho_f \phi}{\rho_s W_0 F(z)} [\lambda_{i-1}c_{i-1}^f(z) - \lambda_i c_i^f(z)] \quad (22)$$

195 which maintain conservation of mass for both fluid and solid individually, and  
 196 do not assume chemical equilibration between the two phases. As above, the  
 197 equations depend on  $F(z)$  and  $D_i(z)$ , i.e. melt fractions and bulk rock partition  
 198 coefficients that can vary with depth.

199 As above, the solid and fluid concentration equations are rewritten in terms of the  
 200 logs of the concentrations:

$$201 \quad U_i^s(z) = \ln \left( \frac{c_i^s(z)}{c_{i,0}^s} \right), \quad U_i^f(z) = \ln \left( \frac{c_i^f(z)}{c_{i,0}^f} \right) \quad (23)$$

202 and thus

$$203 \quad \frac{dU_i}{dz} = \frac{1}{c_i(z)} \frac{dc_i}{dz} \quad (24)$$

204 We assume that initial  $c_{i,0}^s = D_{i,0} c_{i,0}^f$ . Also as above, the log concentration equa-  
 205 tions can be broken into stable and radiogenic components, where the stable log  
 206 concentration equations are:

$$207 \quad \frac{dU_i^{s,stable}}{dz} = \frac{1 - \frac{1}{D_i(z)}}{1 - F(z)} \frac{dF}{dz} \quad (25)$$

$$208 \quad \frac{dU_i^{f,stable}}{dz} = \frac{\frac{D_i^0}{D_i(z)} \exp(U_i^s(z) - U_i^f(z))}{F(z)} \frac{dF}{dz} \quad (26)$$

209 which are equivalent to a model for a fractionally melted residual solid and an  
 210 accumulated fractional melt for the liquid.

211 Reincorporating this with the radiogenic component and scaling all distances by  $h$   
 212 gives the dimensionless equations:

$$213 \quad \frac{dU_i^s}{d\zeta} = \frac{1 - \frac{1}{D_i(\zeta)}}{1 - F(\zeta)} \frac{dF}{d\zeta} + \frac{1 - \phi}{1 - F(\zeta)} \lambda'_i \left[ \frac{\alpha_{i-1}}{\alpha_i} \exp[U_{i-1}^s(\zeta) - U_i^s(\zeta)] - 1 \right] \quad (27)$$

$$214 \quad \frac{dU_i^f}{d\zeta} = \frac{\frac{D_i^0}{D_i(\zeta)} \exp(U_i^s(\zeta) - U_i^f(\zeta))}{F(\zeta)} + \frac{\rho_f \phi}{\rho_s F(\zeta)} \lambda'_i \left[ \frac{D_i^0 \alpha_{i-1}}{D_{i-1}^0 \alpha_i} \exp[U_{i-1}^f(\zeta) - U_i^f(\zeta)] - 1 \right] \quad (28)$$

### 215 **2.3 Solving for transport with chemical reactivity rates**

216 The two models described above are end members for complete equilibrium and  
 217 complete disequilibrium transport. For stable trace elements, these models pro-  
 218 duce melt compositions that are equivalent to batch melting and accumulated  
 219 fractional melting (e.g., Spiegelman and Elliott, 1993). However, the actual trans-  
 220 port of a reactive fluid (like a melt) through a solid matrix can fall anywhere be-  
 221 tween these end members depending on the rate of transport and re-equilibration  
 222 between melt and solid, which can be sensitive to the mesoscopic geometry of  
 223 melt and solid (e.g., Spiegelman and Kenyon, 1992). In an intermediate scenario,

224 we envision that some reaction occurs, but chemical equilibration is incomplete  
 225 due to slow reaction rates relative to the differential transport rates for the fluid  
 226 and solid. If reaction times are sufficiently rapid to achieve chemical exchange  
 227 over the lengthscale of interest before the liquid segregates, chemical equilibrium  
 228 can be achieved; but for reactions that occur more slowly than effective trans-  
 229 port rates, only partial chemical equilibrium can occur (e.g., Grose and Afonso,  
 230 2019; Iwamori, 1993, 1994; Kogiso et al., 2004; Liang and Liu, 2016; Peate and  
 231 Hawkesworth, 2005; Qin et al., 1992; Yang et al., 2000). Such reaction rates can in-  
 232 clude, for example, the rate of chemical migration over the distance between high  
 233 porosity veins or channels (e.g., Aharonov et al., 1995; Jull et al., 2002; Spiegelman  
 234 et al., 2001; Stracke and Bourdon, 2009); or, at the grain scale, the solid chemical  
 235 diffusivity of elements over the diameter of individual mineral grains (e.g., Qin  
 236 et al., 1992; Feineman and DePaolo, 2003; Grose and Afonso, 2019; Oliveira et al.,  
 237 2020; Van Orman et al., 2002a, 2006).

238 To model this scaled reactivity scenario, we start with our equations for disequi-  
 239 librium transport in a steady-state, one-dimensional conservative system, and  
 240 add a chemical back-reaction term that permits exchange of elements between the  
 241 fluid and the solid. The reaction term is scaled by a reactivity rate factor,  $\mathfrak{R}$  and  
 242 expressed in  $\text{kg}/\text{m}^3/\text{yr}$ . (i.e., the same units as the melting rate). The reactivity  
 243 rate thus behaves much like the melting rate by governing the rate of exchange  
 244 between the solid and liquid phases, effectively scaling the degree to which chem-  
 245 ical exchange can occur. This new term could simulate a number of plausible  
 246 scenarios that would physically limit the rate of chemical exchange by transport  
 247 along a given distance in a linear manner, such as the movement or diffusion of  
 248 nuclides through the porous solid matrix between melt channels a given distance  
 249 apart.

250 First, returning to the conservation of mass equations for a steady-state, one-  
 251 dimensional, reactive system of stable trace elements, and using  $\Gamma(z)$  to represent  
 252 the melting rate:

$$253 \quad \frac{d}{dz} \rho_f \phi w = \Gamma(z) \quad (29)$$

$$254 \quad \frac{d}{dz} \rho_s (1 - \phi) W = -\Gamma(z) \quad (30)$$

$$255 \quad \frac{d}{dz} \rho_f \phi w c_i^f(z) = \frac{c_i^s(z)}{D_i(z)} \Gamma(z) - \mathfrak{R} \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (31)$$

$$256 \quad \frac{d}{dz} \rho_s (1 - \phi) W c_i^s(z) = -\frac{c_i^s(z)}{D_i(z)} \Gamma(z) + \mathfrak{R} \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (32)$$

257 where, for an adiabatic upwelling column,

$$258 \quad \Gamma(z) = \rho_s W_0 \frac{dF}{dz} \quad (33)$$

259 From this, the equations (29) and (30) can be integrated (with appropriate bound-  
 260 ary conditions at  $z = 0$ ) to give

$$261 \quad \rho_f \phi w = \rho_s W_0 F(z) \quad (34)$$

$$262 \quad \rho_s(1 - \phi)W = \rho_s W_0(1 - F(z)) \quad (35)$$

263 Next, we expand the concentration equations to include the reactivity factor, and  
 264 substitute the conservation of total mass determined above:

$$265 \quad \rho_s W_0 F(z) \frac{d}{dz} c_i^f(z) + c_i^f(z) \Gamma(z) = \frac{c_i^s(z)}{D_i(z)} \Gamma(z) - \Re \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (36)$$

$$266 \quad \rho_s W_0(1 - F(z)) \frac{d}{dz} c_i^s(z) - c_i^s(z) \Gamma(z) = -\frac{c_i^s(z)}{D_i(z)} \Gamma(z) + \Re \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (37)$$

267 If we then combine the  $\Gamma(z)$  terms and rearrange:

$$268 \quad \rho_s W_0 F(z) \frac{d}{dz} c_i^f(z) = \Gamma(z) \left( \frac{c_i^s(z)}{D_i(z)} - c_i^f(z) \right) - \Re \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (38)$$

$$269 \quad \rho_s W_0(1 - F(z)) \frac{d}{dz} c_i^s(z) = \Gamma(z) c_i^s(z) \left( 1 - \frac{1}{D_i(z)} \right) + \Re \left( c_i^f(z) - \frac{c_i^s(z)}{D_i(z)} \right) \quad (39)$$

270 We can now divide the fluid and solid equations by  $c_i^f$  and  $c_i^s$ , respectively, and  
 271 rearrange the  $W_0$  terms:

$$272 \quad \frac{1}{c_i^f(z)} \frac{dc_i^f}{dz} = \frac{1}{\rho_s W_0 F(z)} \left[ \Gamma(z) \left( \frac{c_i^s(z)}{D_i(z) c_i^f(z)} - 1 \right) - \Re \left( 1 - \frac{c_i^s(z)}{D_i(z) c_i^f(z)} \right) \right] \quad (40)$$

$$273 \quad \frac{1}{c_i^s(z)} \frac{dc_i^s}{dz} = \frac{1}{\rho_s W_0(1 - F(z))} \left[ \Gamma(z) \left( 1 - \frac{1}{D_i(z)} \right) + \frac{\Re}{D_i(z)} \left( \frac{D_i(z) c_i^f(z)}{c_i^s(z)} - 1 \right) \right] \quad (41)$$

274 The first terms on the right-hand side of each of these equations are identical to  
 275 pure disequilibrium melting, such that if  $\Re$  is zero, the equations reduce to the  
 276 disequilibrium transport case of Spiegelman and Elliott (1993).

277 To solve, the final terms that involve the reactivity factor can be further rewritten  
 278 using the definitions for  $U_i^f$  and  $U_i^s$ :

$$279 \quad c_i^f(z) = c_{i,0}^f \exp[U_i^f(z)] = \frac{c_{i,0}^s}{D_i^0} \exp[U_i^f(z)] \quad (42)$$

$$280 \quad c_i^s(z) = c_{i,0}^s \exp[U_i^s(z)] \quad (43)$$

281 Thus:

$$282 \quad \frac{D_i(z) c_i^f(z)}{c_i^s(z)} = \frac{D_i(z)}{D_i^0} \exp[U_i^f(z) - U_i^s(z)] \quad (44)$$

$$\frac{c_i^s(z)}{D_i(z)c_i^f(z)} = \frac{D_i^0}{D_i(z)} \exp[U_i^s(z) - U_i^f(z)] \quad (45)$$

and:

$$\frac{dU_i^f}{dz} = \frac{1}{\rho_s W_0 F(z)} \left[ \Gamma(z) \left( \frac{D_i^0}{D_i(z)} \exp[U_i^s(z) - U_i^f(z)] - 1 \right) - \Re \left( 1 - \frac{D_i^0}{D_i(z)} \exp[U_i^s(z) - U_i^f(z)] \right) \right] \quad (46)$$

$$\frac{dU_i^s}{dz} = \frac{1}{\rho_s W_0 (1 - F(z))} \left[ \Gamma(z) \left( 1 - \frac{1}{D_i(z)} \right) + \frac{\Re}{D_i(z)} \left( \frac{D_i(z)}{D_i^0} \exp[U_i^f(z) - U_i^s(z)] - 1 \right) \right] \quad (47)$$

Finally, substituting adiabatic upwelling and scaling with depth by  $h$ , and adding radioactive terms gives the full solutions for the dimensionless equations  $dU_i/d\zeta$ :

$$\frac{dU_i^f}{d\zeta} = \frac{1}{F(\zeta)} \left[ \frac{dF}{d\zeta} \left( \frac{D_i^0}{D_i(\zeta)} \exp[U_i^s(\zeta) - U_i^f(\zeta)] - 1 \right) \right] - \frac{\Re h}{\rho_s W_0 F(\zeta)} \left[ 1 - \frac{D_i^0}{D_i(\zeta)} \exp[U_i^s(\zeta) - U_i^f(\zeta)] \right] + \frac{\rho_f \phi}{\rho_s F} \lambda_i' \left[ \frac{D_i^0 \alpha_{i-1}}{D_{i-1}^0 \alpha_i} \exp[U_{i-1}^f(\zeta) - U_i^f(\zeta)] - 1 \right] \quad (48)$$

$$\frac{dU_i^s}{d\zeta} = \frac{1}{(1 - F(\zeta))} \left[ \frac{dF}{d\zeta} \left( 1 - \frac{1}{D_i(\zeta)} \right) \right] + \frac{\Re h}{\rho_s W_0 D_i(\zeta) (1 - F(\zeta))} \left[ \frac{D_i(\zeta)}{D_i^0} \exp[U_i^f(\zeta) - U_i^s(\zeta)] - 1 \right] + \frac{1 - \phi}{1 - F(\zeta)} \lambda_i' \left[ \frac{\alpha_{i-1}}{\alpha_i} \exp[U_{i-1}^s(\zeta) - U_i^s(\zeta)] - 1 \right] \quad (49)$$

where  $h$  is the total height of the melting column.

### 2.3.1 The Dahmköhler number

The dimensionless combination

$$Da = \frac{\Re h}{\rho_s W_0} \quad (50)$$

is the Dahmköhler number, which governs the reaction rate relative to the solid transport time. If re-equilibration is limited by solid state diffusion,  $\Re$  can be estimated using:

$$\Re \approx \frac{\rho_s \mathcal{D}_i}{d^2} \quad (51)$$

where  $\mathcal{D}_i$  is the *solid state* diffusivity of element  $i$ , and  $d$  is a nominal spacing between melt-channels (this spacing could, for example, be the average grain diameter for grain-scale channels, or 10 cm for closely spaced veins).

302 In this case (which we will assume for this paper), the Dahmköhler number can  
 303 be written

$$304 \quad Da = \frac{D_i h}{W_0 d^2} \quad (52)$$

305 Substituting the definition of  $Da$  above yields the final dimensionless ODEs for  
 306 the disequilibrium transport model:

$$307 \quad \frac{dU_i^f}{d\zeta} = \frac{1}{F(\zeta)} \left( \frac{dF}{d\zeta} + Da \right) \left( \frac{D_i^0}{D_i(\zeta)} \exp[U_i^s(\zeta) - U_i^f(\zeta)] - 1 \right) + \frac{\rho_f \phi}{\rho_s F(\zeta)} \lambda'_i \left[ \frac{D_i^0 \alpha_{i-1}}{D_{i-1}^0 \alpha_i} \exp[U_{i-1}^f(\zeta) - U_i^f(\zeta)] - 1 \right] \quad (53)$$

$$308 \quad \frac{dU_i^s}{d\zeta} = \frac{1}{(1 - F(\zeta))} \left[ \frac{dF}{d\zeta} \left( 1 - \frac{1}{D_i(\zeta)} \right) + \frac{Da}{D_i(\zeta)} \left( \frac{D_i(\zeta)}{D_i^0} \exp[U_i^f(\zeta) - U_i^s(\zeta)] - 1 \right) \right] + \quad (54)$$

$$\frac{1 - \phi}{1 - F(\zeta)} \lambda'_i \left[ \frac{\alpha_{i-1}}{\alpha_i} \exp[U_{i-1}^s(\zeta) - U_i^s(\zeta)] - 1 \right]$$

309 with initial conditions  $U_i^s = U_i^f = 0$ .

310 In the limit where the Dahmköhler number approaches zero, the above formulas  
 311 reduce to pure disequilibrium transport, whereas if  $Da$  approaches infinity (i.e.,  
 312 infinitely fast reactivity compared to physical transport), the system approaches  
 313 equilibrium conditions ( $c_i^s \rightarrow D_i c_i^f$ ).

### 314 2.3.2 Initial conditions

315 Inspection of equation (53) shows that for the initial conditions described above  
 316 and  $F(0) = 0$ ,  $\frac{dU_i^f}{d\zeta}$  is ill-defined (at least numerically in a floating-point system).  
 317 However, taking the limit  $\zeta \rightarrow 0$  and applying L'Hôpital's rule yields

$$318 \quad \lim_{\zeta \rightarrow 0} \frac{dU_i^f}{d\zeta} = \frac{U_i^s(0) - U_i^f(0)}{F'(0)} \left( \frac{dF}{d\zeta} + Da \right) + \lambda'_i \left[ \frac{D_i^0 \alpha_{i-1}}{D_{i-1}^0 \alpha_i} - 1 \right] \quad (55)$$

319 where

$$320 \quad U_i^s(0) = \left. \frac{dU_i^s}{d\zeta} \right|_{\zeta=0} \quad (56)$$

$$321 \quad U_i^f(0) = \left. \frac{dU_i^f}{d\zeta} \right|_{\zeta=0} \quad (57)$$

$$322 \quad F'(0) = \left. \frac{dF}{d\zeta} \right|_{\zeta=0} \quad (58)$$

323 The initial radiogenic term also uses the limit from equation (34):

$$\lim_{\zeta \rightarrow 0} \frac{\rho_f \phi}{\rho_s F} = \frac{W_0}{w(0)} = 1 \quad (59)$$

Rearranging equation (55) gives the value for  $U_i^f(0)$  for  $F = 0$  as

$$\lim_{\zeta \rightarrow 0} \frac{dU_i^f}{d\zeta} = \frac{1}{2 + \frac{Da}{F'(0)}} \left[ U_i^s(0) \left( 1 + \frac{Da}{F'(0)} \right) + \lambda_i' \left[ \frac{D_i^0 \alpha_{i-1}}{D_{i-1}^0 \alpha_i} - 1 \right] \right] \quad (60)$$

### 3 A pyUserCalc Jupyter notebook

#### 3.1 Code design

The `UserCalc` Python package implements both equilibrium and disequilibrium transport models and provides a set of code classes and utility functions for calculating and visualizing the results of one-dimensional, steady-state, partial melting forward models for both the  $^{238}\text{U}$  and  $^{235}\text{U}$  decay chains. The code package is organized into a set of Python classes and plotting routines, which are documented in the docstrings of the classes and also demonstrated in detail below. Here we briefly describe the overall functionality and design of the code, which is open-source and can be modified to suit an individual researcher's needs. The code is currently available in a Git repository (<https://gitlab.com/ENKI-portal/pyUsercalc>), and any future edits or merge requests will be managed through GitLab.

The equilibrium and disequilibrium transport models described above have each been implemented as Python classes with a generic code interface:

```

342  ...
343  Interface:
344  -----
345      model(alpha0, lambdas, D, W0, F, dFdz, phi, rho_f=2800., rho_s=3300.,
346            method=method, Da=inf)
347
348  Parameters:
349  -----
350      alpha0 : numpy array of initial activities
351      lambdas : numpy array of decay constants scaled by solid transport
352              time
353      D      : Function D(z) -- returns an array of partition coefficients
354              at scaled height z
355      W0     : float -- Solid mantle upwelling rate
356      F      : Function F(z) -- returns the degree of melting F
357      dFdz   : Function dFdz(z) -- returns the derivative of F
358      phi    : Function phi(z) -- returns the porosity
359      rho_f  : float -- melt density
360      rho_s  : float -- solid density
361      method : string -- ODE time-stepping scheme to be passed to
362              solve_ivp (one of 'RK45', 'Radau', 'BDF')
363      Da     : float -- Dahmkohler Number (defaults to \inf, unused in
364              equilibrium model)
365
366  Required Method:
367  -----
368      model.solve(): returns depth and log concentration numpy arrays z,
369      Us, Uf

```

370

371 which solves the scaled equations (i.e., equation (9) or equations (53) and (54) for  
 372 the log concentrations of nuclides  $U_i^f$  and  $U_i^s$  in a decay chain of arbitrary length,  
 373 with scaled decay constants  $\lambda_i'$  and initial activity ratios  $\alpha_0$ . In the code, we use the  
 374 variable  $z$  for the scaled height in the column (i.e.  $z \equiv \zeta$ ), and the model equations  
 375 assume a one-dimensional column with scaled height  $0 \leq z \leq 1$ . The bulk partition  
 376 coefficients  $D_i(z)$ , degree of melting  $F(z)$ , melting rate  $dF/dz(z)$ , and porosity  $\phi(z)$   
 377 are provided as functions of height in the column. Optional arguments include the  
 378 melt and solid densities  $\rho_f$  and  $\rho_s$ , the Dahmköhler number  $Da$ , and the preferred  
 379 numerical integration method (see `scipy.integrate.solve_ivp`). Some of these  
 380 variables, such as  $D_i(z)$  and  $F(z)$ , are provided by the user as described further  
 381 below, and are then interpolated using model functions.

382

`UserCalc` provides two separate model classes, `EquilTransport` and  
 383 `DisequilTransport`, for the different transport models; the user could add any  
 384 other model that uses the same interface, if desired. Most users, however, will not  
 385 access the models directly but rather through the driver class `UserCalc`,  
 386 which provides support for solving and visualizing column models for the relevant  
 387  $^{238}\text{U}$  and  $^{235}\text{U}$  decay chains. The general interface for the `UserCalc` class is:

388

```
389 A class for constructing solutions for 1-D, steady-state, open-system
390 U-series transport calculations as in Spiegelman (2000) and
391 Elkins and Spiegelman (2021).
```

392

Usage:

393

-----

394

```
395
396     us = UserCalc(df,dPdZ = 0.32373,n = 2.,tol=1.e-6,phi0 = 0.008,
397                 W0 =3.,model=EquilTransport,Da=None,stable=False,
398                 method='Radau')
```

399

Parameters:

400

-----

401

```
402 df : A pandas dataframe with columns ['P','F', Kr','DU','DTh',
403 'DRa','DPa']
```

404

```
404 dPdZ : float -- Pressure gradient, to convert pressure P to
405 depth z
```

406

```
406 n : float -- Permeability exponent
```

407

```
407 tol : float -- Tolerance for the ODE solver
```

408

```
408 phi0 : float -- Reference melt porosity
```

409

```
409 W0 : float -- Upwelling velocity (cm/yr)
```

410

```
410 model : class -- A U-series transport model class (one of
411 EquilTransport or DisequilTransport)
```

412

```
412 Da : float -- Optional Da number for disequilibrium transport model
```

413

```
413 stable : bool
```

414

```
414     True: calculates concentrations for non-radiogenic nuclides with same
415     chemical properties (i.e. sets lambda=0)
```

416

```
416     False: calculates the full radiogenic problem
```

417

```
417 method : string
```

418

```
418     ODE time-stepping method to pass to solve_ivp (usually one of 'Radau',
419     'BDF', or 'RK45')
```

420

----

421 The principal required input is a spreadsheet containing the degree of melting  $F(P)$ ,  
 422 relative permeability  $K_r(P)$ , and bulk partition coefficients for the elements  $D_U$ ,  
 423  $D_{Th}$ ,  $D_{Ra}$  and  $D_{Pa}$  as functions of pressure  $P$ . The structure of the input data spread-  
 424 sheet is the same as that described in Spiegelman (2000), and is illustrated in Table  
 425 2 below. Because the user provides  $F(z)$ ,  $K_r(z)$ , and bulk solid  $D_i(z)$  input informa-  
 426 tion to the model directly, any considerations such as mineral modes, mineral/melt  
 427  $D_i$  values, and productivity variations are external to this model and must be de-  
 428 veloped by the user separately. Once given this spreadsheet by the user, the code  
 429 routine initializes the decay constants for the isotopic decay chains and provides  
 430 functions to interpolate  $F(z)$  and  $D_i(z)$  and calculate the porosity  $\phi(z)$ . Once thus  
 431 initialized, the `UserCalc` class further provides the following methods:

```

432     ...
433     Principal Methods:
434     -----
435     phi                : returns porosity as a function of column
436                        height
437     set_column_parameters : resets principal column parameters
438                        phi0, n, W0
439     solve_1D           : 1D column solution for a single Decay
440                        chain with arbitrary D, lambda, alpha_0
441     solve_all_1D       : Solves a single column model for both 238U
442                        and 235U chains.
443                        returns a pandas dataframe
444     solve_grid         : Solves multiple column models for a grid
445                        of porosities and upwelling rates
446                        returns a 3-D array of activity ratios
447     ...
  
```

448 Of these, the principal user-facing methods are:

- 449 1. `UserCalc.solve_all_1D`, which returns a `pandas.DataFrame` table that  
 450 contains, at each depth, solutions for the porosity ( $\phi$ ), the log concentrations  
 451 of the specified nuclides in the  $^{238}\text{U}$  and  $^{235}\text{U}$  decay chains in both the melt  
 452 and the solid, and the U-series activity ratios.
- 453 2. `UserCalc.solve_grid`, which solves for a grid of one-dimensional solutions  
 454 for different reference porosities ( $\phi_0$ ) and solid upwelling rates ( $W_0$ ) and  
 455 returns arrays of U-series activity ratios at a specified depth (usually the top  
 456 of the column), as described in Spiegelman and Elliott (1993).

### 457 3.1.1 Visualization Functions

458 In addition to the principal classes for calculating U-series activity ratios in partial  
 459 melts, the `UserCalc` package also provides functions for visualizing model inputs  
 460 and outputs. The primary plotting functions include:

- 461 1. `UserCalc.plot_inputs(df)` : Visualizes the input dataframe to show  $F(P)$ ,  
 462  $K_r(P)$  and  $D_i(P)$ .
- 463 2. `UserCalc.plot_1Dcolumn(df)` : Visualizes the output dataframe for a single  
 464 one-dimensional melting column.
- 465 3. `UserCalc.plot_contours(phi0,W0,act)` : Visualizes the output of  
 466 `UserCalc.solve_grid` by generating contour plots of activity ratios at a  
 467 specific depth as functions of the porosity ( $\phi_0$ ) and solid upwelling rate ( $W_0$ ).

468 4. `UserCalc.plot_mesh_Ra(Th,Ra,W0,phi0)` and `UserCalc.plot_mesh_Pa(Th,Pa,W0,phi0)` :  
 469 Generates 'mesh' plots showing results for different  $\phi_0$  and  $W_0$  values on  
 470 ( $^{226}\text{Ra}/^{230}\text{Th}$ ) vs. ( $^{230}\text{Th}/^{238}\text{U}$ ) and ( $^{231}\text{Pa}/^{235}\text{U}$ ) vs. ( $^{230}\text{Th}/^{238}\text{U}$ ) activity  
 471 diagrams.

472 Both the primary solver routines and visualization routines will be demonstrated in  
 473 detail below.

### 474 3.1.2 Miscellaneous Convenience Functions

475 Finally, the UserCalc module also provides a simple input spreadsheet generator  
 476 similar to the one provided with the original UserCalc program of Spiegelman  
 477 (2000). This tool is described more fully in the accompanying Jupyter notebook  
 478 `twolayermodel.ipynb` in the Supplemental Materials, and has the interface:

```
479 df = UserCalc.twolayermodel(P, F, Kr, D_lower, D_upper, N=100, P_lambda=1)
```

## 480 3.2 An example demonstrating pyUserCalc functionality for a single melting 481 column

482 The Python code cells embedded below provide an example problem that demon-  
 483 strates the use and behavior of the model for a simple, two-layer upwelling mantle  
 484 column, with a constant melting rate within each layer and constant  $K_r = 1$ . This  
 485 example is used to compare the outcomes from the original UserCalc equilibrium  
 486 model (Spiegelman, 2000) to various other implementations of the code, such as  
 487 pure disequilibrium transport and scaled reactivity rates, as described above.

488 To run the example code and use this article as a functioning Jupyter notebook,  
 489 while in a web-enabled browser the user should select an embedded code cell by  
 490 mouse-click and then simultaneously type the 'Shift' and 'Enter' keys to run the cell,  
 491 after which selection will automatically advance to the following cell. The first cell  
 492 below imports necessary code libraries to access the Python toolboxes and functions  
 493 that will be used in the rest of the program:

```
[1]: # Select this cell with by mouseclick, and run the code by simultaneously ↵
      ↪ typing the 'Shift' + 'Enter' keys.
      # If the browser is able to run the Jupyter notebook, a number [1] will ↵
      ↪ appear to the left of the cell.

import pandas as pd
import numpy as np
import matplotlib.pyplot as plt
%matplotlib inline

# Import UserCalc:
import UserCalc
```

### 494 3.2.1 Entering initial input information and viewing input data

495 In the full Jupyter notebook code available in the Git repository and provided here  
 496 as Supplementary Materials, the user can edit a notebook copy and indicate their  
 497 initial input data, as has been done for the sample data set below. The name for the  
 498 user's input data file should be set in quotes (i.e., replacing the word 'sample' in  
 499 the cell below with the appropriate filename, minus the file extension). This name  
 500 will be used both to find the input file and to label any output files produced. Our  
 501 sample file can likewise be downloaded and used as a formatting template for other  
 502 input files (see Supplementary Materials), and is presented as a useful example  
 503 below. The desired input file should be saved to a 'data' folder in the notebook di-  
 504

505 rectory prior to running the code. If desired, a similarly simple two-layer input file  
506 can also be generated using the calculator tool provided in the supplementary code.

507 Once the cell has been edited to contain the correct input file name, the user should  
508 run the cell using the technique described above:

```
509 [2]: runname='sample'
```

510 The next cell below will read in the input data using the user filename specified  
511 above:

```
512 [3]: input_file = 'data/{}.csv'.format(runname)  
df = pd.read_csv(input_file, skiprows=1, dtype=float)  
df
```

Table 2: Input data table for example tested here, showing pressures in kbar ( $P$ ), degree of melting ( $F$ ), permeability coefficient ( $K_r$ ), and bulk solid/melt partition coefficients ( $D_i$ ) for the elements of interest, U, Th, Ra, and Pa. This table illustrates the format required for input files for this model.

	P	F	Kr	DU	DTh	DRa	DPa
0	40.0	0.00000	1.0	0.00900	0.00500	0.00002	0.00001
1	39.0	0.00241	1.0	0.00900	0.00500	0.00002	0.00001
2	38.0	0.00482	1.0	0.00900	0.00500	0.00002	0.00001
3	37.0	0.00723	1.0	0.00900	0.00500	0.00002	0.00001
4	36.0	0.00964	1.0	0.00900	0.00500	0.00002	0.00001
5	35.0	0.01210	1.0	0.00900	0.00500	0.00002	0.00001
6	34.0	0.01450	1.0	0.00900	0.00500	0.00002	0.00001
7	33.0	0.01690	1.0	0.00900	0.00500	0.00002	0.00001
8	32.0	0.01930	1.0	0.00900	0.00500	0.00002	0.00001
9	31.0	0.02170	1.0	0.00900	0.00500	0.00002	0.00001
10	30.0	0.02410	1.0	0.00900	0.00500	0.00002	0.00001
11	29.0	0.02650	1.0	0.00900	0.00500	0.00002	0.00001
12	28.0	0.02890	1.0	0.00900	0.00500	0.00002	0.00001
13	27.0	0.03130	1.0	0.00900	0.00500	0.00002	0.00001
14	26.0	0.03370	1.0	0.00900	0.00500	0.00002	0.00001
15	25.0	0.03620	1.0	0.00900	0.00500	0.00002	0.00001
16	24.0	0.03860	1.0	0.00900	0.00500	0.00002	0.00001
17	23.0	0.04100	1.0	0.00899	0.00500	0.00002	0.00001
18	22.0	0.04340	1.0	0.00893	0.00498	0.00002	0.00001
19	21.0	0.04610	1.0	0.00852	0.00488	0.00002	0.00001
20	20.0	0.05000	1.0	0.00700	0.00450	0.00002	0.00001
21	19.0	0.05610	1.0	0.00548	0.00412	0.00002	0.00001
22	18.0	0.06340	1.0	0.00507	0.00402	0.00002	0.00001
23	17.0	0.07100	1.0	0.00501	0.00400	0.00002	0.00001
24	16.0	0.07860	1.0	0.00500	0.00400	0.00002	0.00001
25	15.0	0.08620	1.0	0.00500	0.00400	0.00002	0.00001
26	14.0	0.09370	1.0	0.00500	0.00400	0.00002	0.00001
27	13.0	0.10133	1.0	0.00500	0.00400	0.00002	0.00001
28	12.0	0.10892	1.0	0.00500	0.00400	0.00002	0.00001
29	11.0	0.11651	1.0	0.00500	0.00400	0.00002	0.00001
30	10.0	0.12410	1.0	0.00500	0.00400	0.00002	0.00001
31	9.0	0.13169	1.0	0.00500	0.00400	0.00002	0.00001
32	8.0	0.13928	1.0	0.00500	0.00400	0.00002	0.00001
33	7.0	0.14687	1.0	0.00500	0.00400	0.00002	0.00001
34	6.0	0.15446	1.0	0.00500	0.00400	0.00002	0.00001
35	5.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
36	4.0	0.16964	1.0	0.00500	0.00400	0.00002	0.00001
37	3.0	0.17723	1.0	0.00500	0.00400	0.00002	0.00001
38	2.0	0.18482	1.0	0.00500	0.00400	0.00002	0.00001
39	1.0	0.19241	1.0	0.00500	0.00400	0.00002	0.00001
40	0.0	0.20000	1.0	0.00500	0.00400	0.00002	0.00001

513 The next cell will visualize the input dataframe in Figure 1, using the utility function  
514 `plot_inputs` :

```
[4]: fig = UserCalc.plot_inputs(df)
```

515

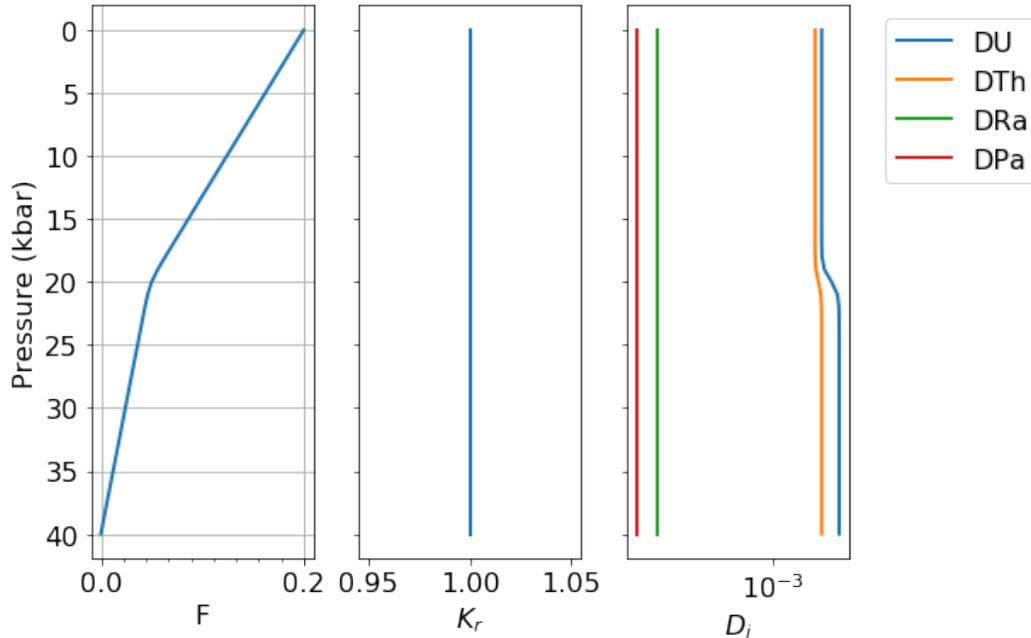


Figure 1: Diagrams showing example input parameters  $F$ ,  $K_r$ , and  $D_i$  as a function of pressure, for the sample input file tested here.

### 516 3.2.2 Single column equilibrium transport model

517 In its default mode, `UserCalc` solves the one-dimensional steady-state equilibrium  
 518 transport model described in Spiegelman (2000). Below we will initialize the model,  
 519 solve for a single column and plot the results.

520 First we set the physical parameters for the upwelling column and initial conditions:

```
[5]: # Maximum melt porosity:
phi0 = 0.008

# Solid upwelling rate in cm/yr. (to be converted to km/yr. in the driver_
  ↪function):
W0 = 3.

# Permeability exponent:
n = 2.

# Solid and liquid densities in kg/m3:
rho_s = 3300.
rho_f = 2800.

# Initial activity values (default is 1.0):
alpha0_238U = 1.
alpha0_235U = 1.
```

521

```

alpha0_230Th = 1.
alpha0_226Ra = 1.
alpha0_231Pa = 1.
alpha0_all = np.array([alpha0_238U, alpha0_230Th, alpha0_226Ra,
→alpha0_235U, alpha0_231Pa])

```

522

523 Next, we initialize the default equilibrium model:

```
[6]: us_eq = UserCalc.UserCalc(df)
```

524

525 and run the model for the input code and display the results for the final predicted  
526 melt composition in List 1:

```
[7]: df_out_eq = us_eq.solve_all_1D(phi0,n,W0,alpha0_all)
df_out_eq.tail(n=1)
```

527

```
[7]:
      P      z      F      phi (230Th/238U) (226Ra/230Th) (231Pa/235U) Uf_238U
40  0.0  0.0  0.2  0.008  1.164941    1.590091    2.10557   -3.121055

      Uf_230Th Uf_226Ra  Us_238U  Us_230Th  Us_226Ra  Uf_235U  Uf_231Pa
40 -3.556171 -8.613841 -3.121055 -3.556171 -8.613841 -3.121909 -9.179718

      Us_235U  Us_231Pa
40 -3.121909 -9.179718
```

528

529 **List 1.** Model output results for the equilibrium melting scenario tested above.

530 The cell below produces Figure 2, which shows the model results with depth:

```
[8]: fig = UserCalc.plot_1Dcolumn(df_out_eq)
```

531



```
[11]: fig, axes = UserCalc.plot_1Dcolumn(df_out)
for s in ['(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']:
    axes[2].plot(df_out_eq[s], df_out['P'], '--', color='grey')
axes[2].set_title('Da = {}'.format(us_diseq.Da))
plt.show()
```

544

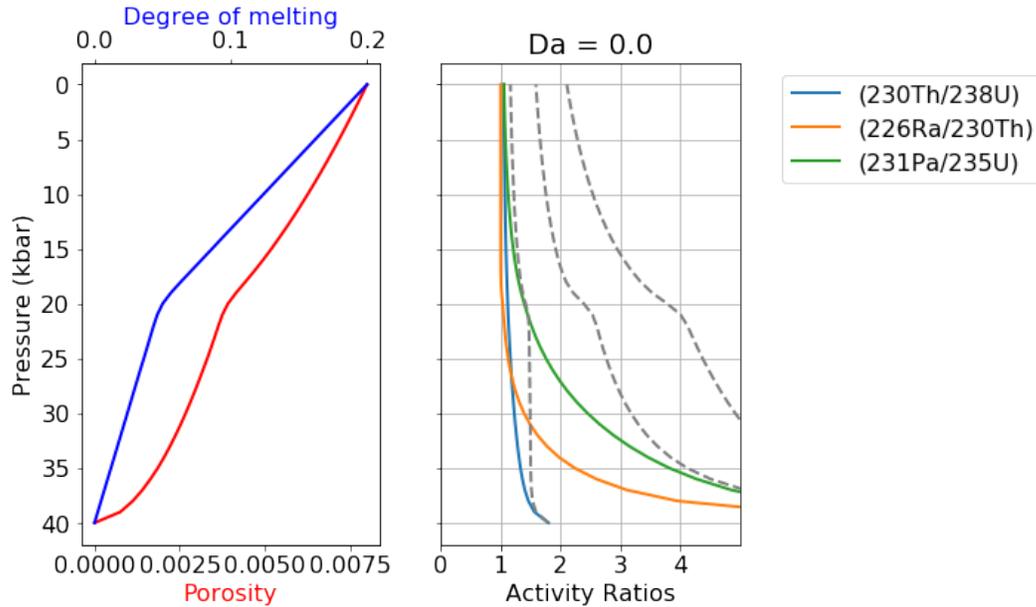


Figure 3: Disequilibrium model output results for the degree of melting, residual melt porosity, and activity ratios ( $^{230}\text{Th}/^{238}\text{U}$ ), ( $^{226}\text{Ra}/^{230}\text{Th}$ ), and ( $^{231}\text{Pa}/^{235}\text{U}$ ) as a function of pressure, for the Dahmköhler number shown ( $Da = 0$ ). For comparison, the dashed grey curves show solutions for the equilibrium transport model.

545 The dashed grey curves in Figure 3 illustrate the equilibrium transport solution,  
 546 which is significantly different from the disequilibrium solution. If we increase the  
 547 value of  $Da$ , however, the disequilibrium transport solution should converge to-  
 548 wards the equilibrium scenario. To illustrate this, below we calculate the result for  
 549  $Da = 1$ :

```
[12]: # Reset the Da number in the reactive transport model to 1:
us_diseq.Da=1.

# Recalculate the model:
df_out = us_diseq.solve_all_1D(phi0,n,W0,alpha0_all)
df_out_eq.tail(n=1)
```

550

```
[12]:      P      z      F      phi (230Th/238U) (226Ra/230Th) (231Pa/235U) Uf_238U
40 0.0  0.0  0.2  0.008  1.164941      1.590091      2.10557 -3.121055

      Uf_230Th Uf_226Ra  Us_238U  Us_230Th  Us_226Ra  Uf_235U  Uf_231Pa
40 -3.556171 -8.613841 -3.121055 -3.556171 -8.613841 -3.121909 -9.179718
```

551

```
Us_235U Us_231Pa
40 -3.121909 -9.179718
```

552

553

554

**List 3.** Model output results for the disequilibrium melting scenario tested above, where  $Da = 1$ .

```
[13]: fig, axes = UserCalc.plot_1Dcolumn(df_out)
for s in ['(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']:
    axes[2].plot(df_out_eq[s], df_out['P'], '--', color='grey')
axes[2].set_title('Da = {}'.format(us_diseq.Da))
plt.show()
```

555

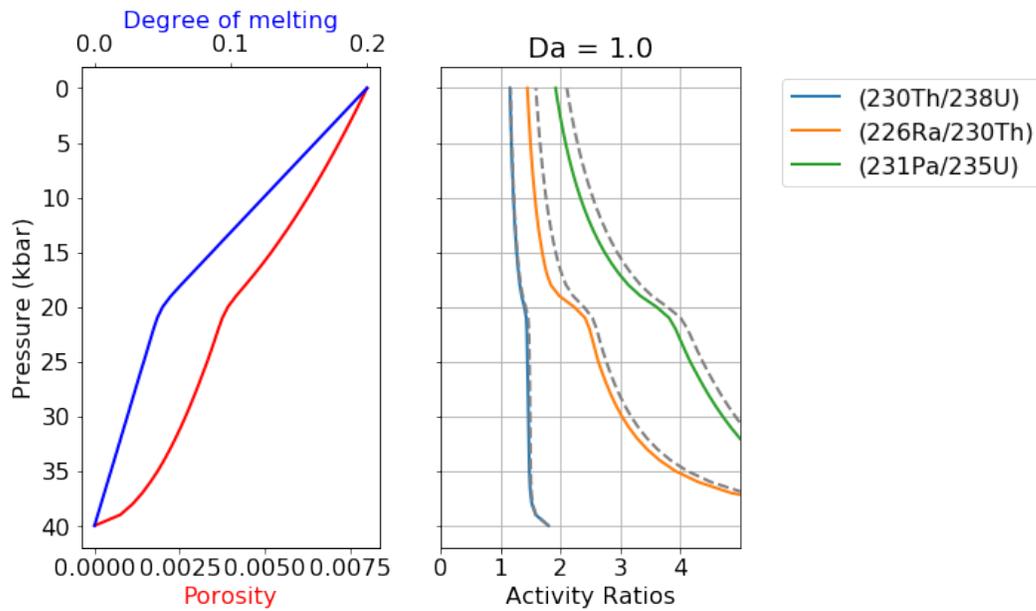


Figure 4: Disequilibrium model output as in Figure 3, but for  $Da = 1$ .

556

557

The outcome of the above calculation (Figure 4, List 3) approaches the equilibrium scenario more closely, as predicted. Below is an additional comparison for  $Da = 10$ :

```
[14]: # Reset the Da number in the reactive transport model to 10:
us_diseq.Da=10.

# Recalculate and plot the model:
df_out = us_diseq.solve_all_1D(phi0,n,W0,alpha0_all)
fig, axes = UserCalc.plot_1Dcolumn(df_out)
for s in ['(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']:
    axes[2].plot(df_out_eq[s], df_out['P'], '--', color='grey')
axes[2].set_title('Da = {}'.format(us_diseq.Da))
plt.show()
```

558

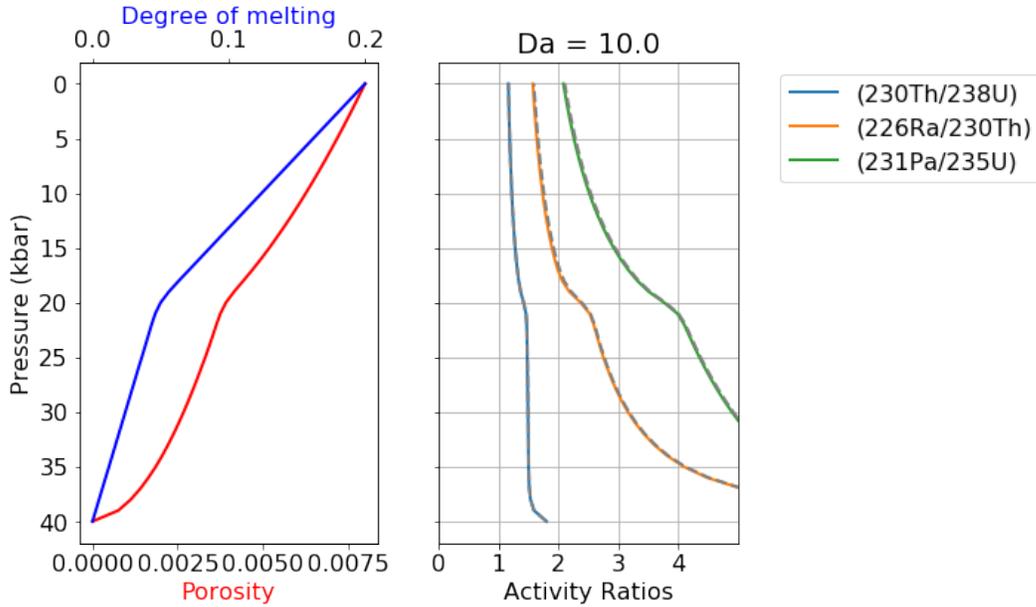


Figure 5: Disequilibrium model output as in Figure 3, but for  $Da = 10$ .

559 For  $Da = 10$  (Figure 5), the activity ratios in the melt are indistinguishable from the  
 560 equilibrium calculation, suggesting that a Damköhler number of 10 is sufficiently  
 561 high for a melting system to approach chemical equilibrium, and illustrating that  
 562 the equilibrium model of Spiegelman and Elliott (1993) and Spiegelman (2000) is  
 563 the limiting case for the more general disequilibrium model presented here. For this  
 564 problem, equilibrium transport always provides an upper bound on activity ratios.

### 565 3.2.4 Stable element concentrations

566 For a stable element, i.e.,  $\lambda_i = 0$ , Spiegelman and Elliott (1993) showed that the  
 567 equilibrium melting model reduces identically to simple batch melting (Shaw, 1970),  
 568 while the disequilibrium model with  $Da = 0$  is equivalent to true fractional melting.  
 569 This presents a useful test of the calculator that verifies the program is correctly calcu-  
 570 lating stable concentrations. To simulate stable element concentrations for U, Th,  
 571 Ra, and Pa during equilibrium melting, we can use the same input file example as  
 572 above and simply test the scenario where  $\lambda_i$  values are equal to zero.

573 First, we impose a "stable" condition that changes all decay constants  $\lambda_i = 0$ :

```
574 [15]: us_eq = UserCalc.UserCalc(df, stable=True)
df_out_eq = us_eq.solve_all_1D(phi0, n, W0, alpha0_all)
df_out_eq.tail(n=1)
```

```
[15]:      P      z      F      phi (230Th/238U) (226Ra/230Th) (231Pa/235U) Uf_238U
40  0.0  0.0  0.2  0.008  1.003937  1.015919  1.019959  -3.120895

      Uf_230Th Uf_226Ra  Us_238U  Us_230Th  Us_226Ra  Uf_235U  Uf_231Pa
40  -3.704753 -9.21042 -3.120895 -3.704753 -9.21042 -3.120895 -9.903528

      Us_235U  Us_231Pa
40  -3.120895 -9.903528
```

575

576 **List 4.** Model output results for equilibrium porous flow melting where  $\lambda_i = 0$ ,  
 577 simulating stable element behavior for U, Th, Ra, and Pa and thus true (instan-  
 578 taneous) batch melting.

579 For comparison with the results in List 4, we can use the batch melting equation  
 580 (Shaw, 1970) to calculate the concentrations of U, Th, Ra, and Pa using the input  
 581 values in Table 2 for  $F(z)$  and  $D_i$ , where:

$$582 \quad \frac{c_i^f}{c_i^0} = \frac{1}{F + D_i(1 - F)} \quad (61)$$

583 and determine radionuclide activities for the batch melt using the definition of the  
 584 activity  $a$  for a nuclide  $i$ :

$$585 \quad a_i = \lambda_i c_i^f \quad (62)$$

586 and the initial nuclide activities  $a_i^0$ , such that:

$$587 \quad a_i = \frac{a_i^0}{F + D_i(1 - F)} \quad (63)$$

588 As the activity ratios in List 5 illustrate, the outcomes of this simple batch melting  
 589 equation are identical to those produced by the model for equilibrium transport and  
 590  $\lambda = 0$ .

```

[16]: df_batch=df[['P', 'F', 'DU', 'DTh', 'DRa', 'DPa']]
df_batch['(230Th/238U)'] = (alpha0_all[1]/(df_batch.F-df_batch.F*df_batch.
    ↳DTh+df_batch.DTh))/(alpha0_all[0]/(df_batch.F-df_batch.F*df_batch.
    ↳DU+df_batch.DU))
df_batch['(226Ra/230Th)'] = (alpha0_all[2]/(df_batch.F-df_batch.
    ↳F*df_batch.DRa+df_batch.DRa))/(alpha0_all[1]/(df_batch.F-df_batch.
    ↳F*df_batch.DTh+df_batch.DTh))
df_batch['(231Pa/235U)'] = (alpha0_all[4]/(df_batch.F-df_batch.F*df_batch.
    ↳DPa+df_batch.DPa))/(alpha0_all[3]/(df_batch.F-df_batch.F*df_batch.
    ↳DU+df_batch.DU))

# Extract columns and concatenate dataframes
cols = ['P', 'F', '(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']
df_compare = pd.concat([ df_batch[cols].tail(1), df_out_eq[cols].tail(1)])
df_compare['model'] = ['Batch Melting', 'Equilibrium Transport: stable_
    ↳elements']
df_compare.set_index('model')
591
    
```

[16]:	P	F	(230Th/238U)	(226Ra/230Th)
model				
Batch Melting	0.0	0.2	1.003937	1.015919
Equilibrium Transport: stable elements	0.0	0.2	1.003937	1.015919
			(231Pa/235U)	
model				

592

Batch Melting 1.019959  
 Equilibrium Transport: stable elements 1.019959

593

594 **List 5.** Simple batch melting calculation results using the methods of Shaw  
 595 (1970), demonstrating identical activity ratio results to those calculated using  
 596 the equilibrium transport model with  $\lambda_i = 0$ .

597 Similarly, we can also determine pure disequilibrium melting using the disequilib-  
 598 rium transport model with  $\lambda_i = 0$ . A simple fractional melting problem is easiest  
 599 to test using constant melt productivity and partitioning behavior, so here we test a  
 600 simplified, one-layer scenario with constant  $dF/dz$  and  $D_i$  values:

```
[17]: input_file_2 = 'data/simple_sample.csv'
df_test = pd.read_csv(input_file_2, skiprows=1, dtype=float)
UserCalc.plot_inputs(df_test)
df_test.tail(n=1)
```

601

[17]: P F Kr DU DTh DRa DPa  
 40 0.0 0.0964 1.0 0.009 0.005 0.00002 0.00001

602

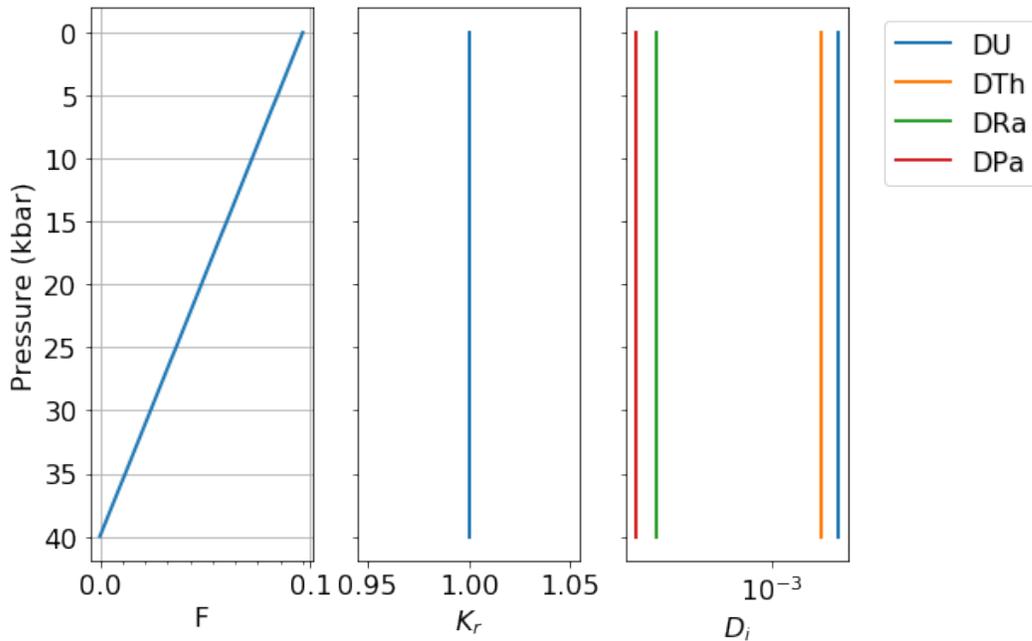


Figure 6: Simple alternative input file with constant melt productivity and constant solid/melt partitioning, used here to test pure fractional melting outputs.

603 We note that numerical ODE solvers may not successfully solve for pure fractional  
 604 melting with  $Da = 0$  and stable elements, because the resulting extreme changes in  
 605 solid concentrations for highly incompatible elements are difficult to resolve using  
 606 numerical methods. Stable solutions can nonetheless be obtained for very small  
 607 values of  $Da$  that approach  $Da = 0$ , and such solutions still provide a useful test

608 of the disequilibrium transport model. Here we use  $Da = 10^{-10}$ ; for such low  $Da$   
 609 values, the liquid closely approaches the composition of an accumulated fractional  
 610 melt, and although the liquid and solid outcomes are slightly different from pure  
 611 fractional melting, the solid is still essentially depleted of all incompatible nuclides.

```
[18]: us_diseq_test = UserCalc.UserCalc(df_test, model=UserCalc.  
      ↪DisequilTransport, stable=True, Da=1.e-10)
```

612

```
[19]: df_diseq_test = us_diseq_test.solve_all_1D(phi0,n,W0,alpha0_all)
```

613

614 Similar to our approach for equilibrium and batch melting, we can compare the  
 615 results of disequilibrium transport for stable elements with pure fractional melting  
 616 for constant partition coefficients using the definition of aggregated fractional melt  
 617 concentrations (Figure 7):

$$618 \quad \frac{c_i^s}{c_i^{s,0}} = (1-F)^{1/D_i-1} \quad (64)$$

$$619 \quad \frac{c_i^f}{c_i^{f,0}} = \frac{D_i}{F} \left( 1 - (1-F)^{1/D_i} \right) \quad (65)$$

620 or in log units:

$$621 \quad U_i^s = (1/D_i - 1) \log(1-F) \quad (66)$$

$$622 \quad U_i^f = \log \left( 1 - (1-F)^{1/D_i} \right) + \log \left( \frac{D_i}{F} \right) \quad (67)$$

```
[20]: df_frac=df_test[['P','F','DU','DTh','DRa','DPa']]  
df_frac['(230Th/238U)'] = ((alpha0_all[1]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DTh))) / ((alpha0_all[0]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DU)))  
df_frac['(226Ra/230Th)'] = ((alpha0_all[2]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DRa))) / ((alpha0_all[1]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DTh)))  
df_frac['(231Pa/235U)'] = ((alpha0_all[4]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DPa))) / ((alpha0_all[3]/df_frac.F)*(1.-(1.-df_frac.  
  ↪F)**(1./df_frac.DU)))
```

623

```
[21]: fig, axes = UserCalc.plot_1Dcolumn(df_diseq_test)  
for s in ['(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']:  
    axes[2].plot(df_frac[s], df_diseq_test['P'], '--', color='black')  
plt.show()
```

624

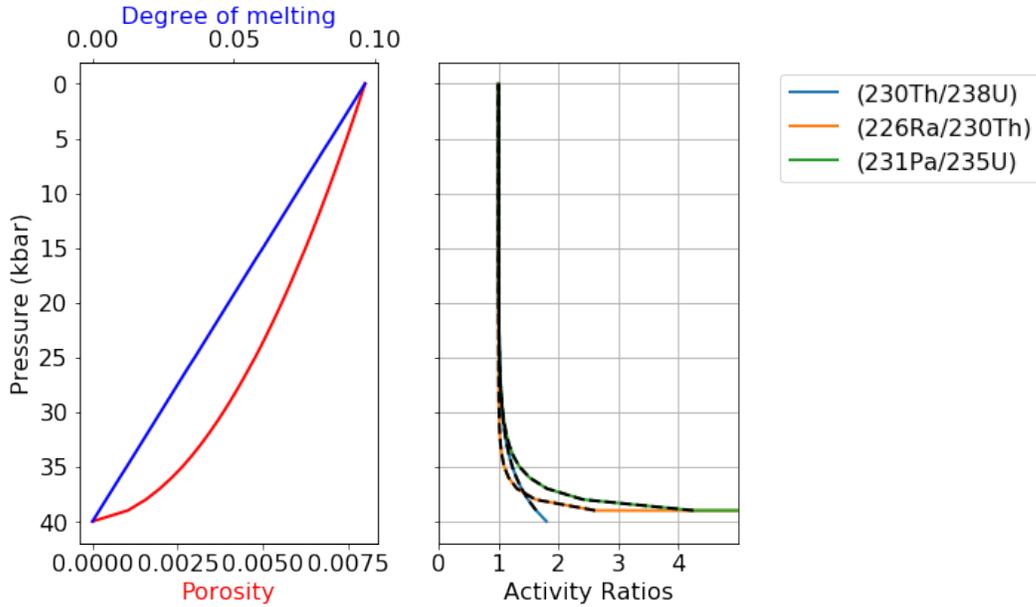


Figure 7: Model output results for the degree of melting, residual melt porosity, and activity ratios ( $^{230}\text{Th}/^{238}\text{U}$ ), ( $^{226}\text{Ra}/^{230}\text{Th}$ ), and ( $^{231}\text{Pa}/^{235}\text{U}$ ) as a function of pressure. The solid curves plot the results of pure fractional melting for stable elements, while the dashed black curves illustrate the outcomes of the disequilibrium transport model with  $Da = 10^{-10}$  and  $\lambda_i = 0$ . The outcomes of the two methods are indistinguishable.

### 625 3.2.5 Considering lithospheric transport scenarios

626 In mantle decompression melting scenarios, melting is expected to cease in the  
 627 shallow, colder part of the regime where a lithospheric layer is present. The effects  
 628 of cessation of melting prior to reaching the surface can be envisioned as affecting  
 629 magma compositions in a number of ways, some of which could be calculated using  
 630 the models presented here by setting  $dF = 0$ .

631 There are, however, several limitations when using our transport models to simulate  
 632 lithospheric melt transport in this way, as the model equations are written to track  
 633 steady-state decompression and melting. The first limitation is thus the underlying  
 634 assumption that the solid is migrating and experiencing progressive melt depletion  
 635 in the model, while the solid lithosphere should in fact behave as a rigid matrix  
 636 that does not experiencing upwelling. For the disequilibrium transport model with  
 637  $Da = 0$ , no chemical reequilibration occurs while  $dF = 0$ , so the lack of solid mi-  
 638 gration after the cessation of melting does not pose a problem; instead, in the pure  
 639 disequilibrium transport case, imposing  $dF = 0$  simply allows for radioactive decay  
 640 and ingrowth during transport through the lithospheric layer.

641 The equilibrium transport model, on the other hand, permits full equilibration  
 642 even if  $dF = 0$ , but the liquid composition does not directly depend on the solid  
 643 concentration,  $c_i^s(z)$ , so ongoing chemical reequilibration between the liquid and a  
 644 modified lithospheric solid could be simulated by modifying the bulk solid/liquid  
 645 partition coefficients  $D_i$ . However, the underlying model assumes that the liquid  
 646 with mass proportion  $F_{max}$  reequilibrates with the solid matrix in a steady-state  
 647 transport regime, at the maximum reference porosity, which may not accurately  
 648 simulate the transport regime through the fixed lithosphere with no melting. Be-  
 649 cause it does not directly consider mineral abundances or compositions, the model

650 also does not account for complexities such as low temperature melt-rock reaction  
651 or mineral growth.

652 The case of the scaled disequilibrium transport model with  $Da > 0$  is the most  
653 complex, since the model directly calculates reequilibration of the liquid with a  
654 progressively melting solid layer, and thus may not accurately simulate transport  
655 through the fixed solid lithosphere. We advise that if the model is used in this way,  
656 the results must be interpreted with additional caution.

657 Finally, calculating a given transport model through the upwelling asthenosphere  
658 and into a fixed overlying lithospheric layer neglects an additional, significant limi-  
659 tation: namely that melt-rock interactions, and thus the magma transport style, may  
660 be different in the lithosphere than in the melting asthenosphere. As noted above,  
661 this could also include low-temperature reactions and the growth of new mineral  
662 phases. While it is not possible to change transport models during a single 1D run  
663 in the current implementation, one alternative approach is to change the relative  
664 permeability,  $K_r$ , in the lithosphere, in addition to modifying the bulk partition co-  
665 efficients to reflect lithospheric values. It may also be possible to run a separate,  
666 second-stage lithospheric calculation with modified input parameters and revised  
667 liquid porosity constraints, but this option is not currently implemented and would  
668 require an expansion of the current model.

669 Despite these caveats, there are some limited scenarios where users may wish to  
670 simulate equilibrium or disequilibrium magma transport through a capping layer  
671 with constant  $dF = 0$ , constant  $\phi = \phi_0$ , and revised  $D_i$  values for a modified layer  
672 mineralogy. The cells below provide options for modifying the existing input data  
673 table to impose such a layer. The first cell identifies a final melting pressure  $P_{Lithos}$ ,  
674 which is defined by the user in kbar. This value can be set to 0.0 if no lithospheric  
675 cap is desired; in the example below, it has been set at 5.0 kbar. There are two overall  
676 options for how this final melting pressure could be used to modify the input data.  
677 The first option (implemented in the Supplementary Materials but not tested here)  
678 simply deletes all lines in the input dataframe for depths shallower than  $P_{Lithos}$ . This  
679 is a straightforward option for a one-dimensional column scenario, where melting  
680 simply stops at the base of the lithosphere and the composition of the melt product  
681 is observed in that position. This is an effective way to limit further chemical inter-  
682 actions after melting has ceased; it fails to account for additional radioactive decay  
683 during lithospheric melt transport, but subsequent isotopic decay over a fixed trans-  
684 port time interval could then be calculated using the radioactive decay equations for  
685 U-series nuclides.

686 A second option, shown here to demonstrate outcomes, changes the degree of melt-  
687 ing increments ( $dF$ ) to a value of 0 for all depths shallower than  $P_{Lithos}$ , but allows  
688 model calculations to continue at shallower depths. This is preferable if the user  
689 aims to track additional radioactive decay and/or chemical exchange after melting  
690 has ceased and during subsequent transport through the lithospheric layer, and  
691 shall be explored further below.

```
692 [22]: Plithos = 5.0

        Pfinal = df.iloc[(df['P']-Plithos).abs().idxmin()]
        F_max = Pfinal[1].tolist()
        df.loc[(df['P'] < Plithos),['F']] = F_max
```

693 For equilibrium transport scenarios, the cell below offers one possible option for  
694 modifying lithospheric solid/melt bulk partition coefficients. We note that if the

695 disequilibrium transport model is used with  $Da = 0$  (i.e., pure chemical disequilibrium)  
 696 ), this cell is not necessary.

697 The option demonstrated below imposes new, constant melt-rock partition coef-  
 698 ficients during lithospheric transport. These values are assumed to be fixed. An  
 699 alternative choice, included in the Supplementary Materials, instead fixes the shal-  
 700 lower lithospheric solid/melt bulk partition coefficients such that they are equal to  
 701  $D_i$  values at the depth where melting ceased (i.e.,  $P_{Lithos}$ ).

```
[23]: # Define new bulk solid/liquid partition coefficients for the
      ↪ lithospheric layer:
      D_U_lith = 0.002
      D_Th_lith = 0.006
      D_Ra_lith = 0.00002
      D_Pa_lith = 0.00001

      # Implement the changed values defined above:
      df.loc[(df['P'] < Plithos),['DU']] = D_U_lith
      df.loc[(df['P'] < Plithos),['DTh']] = D_Th_lith
      df.loc[(df['P'] < Plithos),['DRa']] = D_Ra_lith
      df.loc[(df['P'] < Plithos),['DPa']] = D_Pa_lith
```

702  
 703 Following any changes implemented above, the cells below will process and display  
 704 the refined input data (Figure 8, Table 3).

```
[24]: UserCalc.plot_inputs(df)
```

705

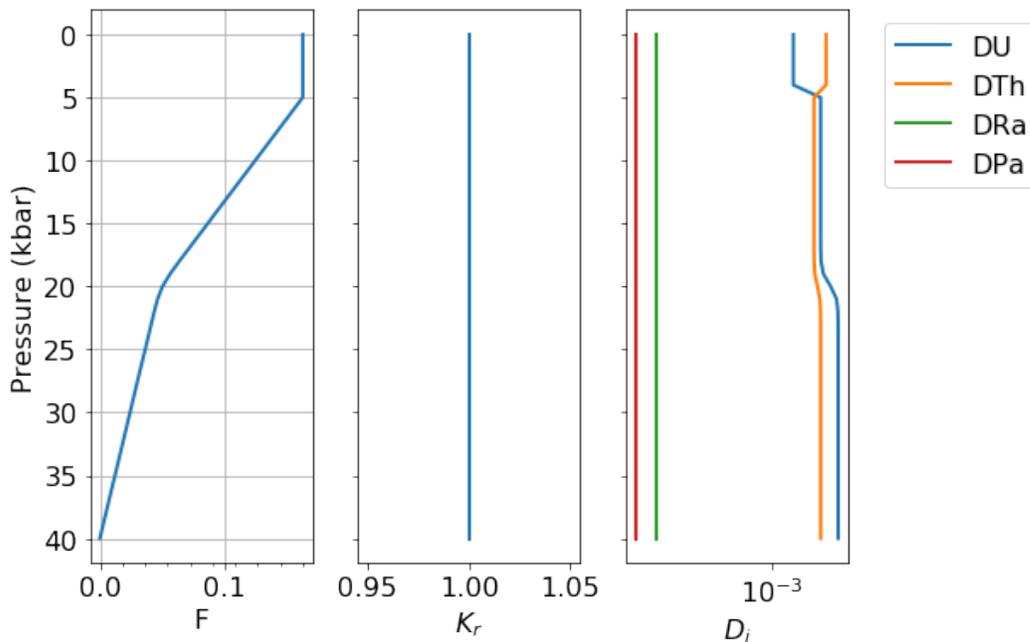


Figure 8: Diagrams showing input parameters  $F$ ,  $K_r$ , and  $D_i$  as a function of pressure, for the example input file and modified lithospheric conditions.

[25] : df

706

Table 3: Input data table for an example scenario with modified lithospheric transport conditions, showing pressures in kbar ( $P$ ), degree of melting ( $F$ ), permeability coefficient ( $K_r$ ), and bulk solid/melt partition coefficients ( $D_i$ ) for the elements of interest, U, Th, Ra, and Pa.

	P	F	Kr	DU	DTh	DRa	DPa
0	40.0	0.00000	1.0	0.00900	0.00500	0.00002	0.00001
1	39.0	0.00241	1.0	0.00900	0.00500	0.00002	0.00001
2	38.0	0.00482	1.0	0.00900	0.00500	0.00002	0.00001
3	37.0	0.00723	1.0	0.00900	0.00500	0.00002	0.00001
4	36.0	0.00964	1.0	0.00900	0.00500	0.00002	0.00001
5	35.0	0.01210	1.0	0.00900	0.00500	0.00002	0.00001
6	34.0	0.01450	1.0	0.00900	0.00500	0.00002	0.00001
7	33.0	0.01690	1.0	0.00900	0.00500	0.00002	0.00001
8	32.0	0.01930	1.0	0.00900	0.00500	0.00002	0.00001
9	31.0	0.02170	1.0	0.00900	0.00500	0.00002	0.00001
10	30.0	0.02410	1.0	0.00900	0.00500	0.00002	0.00001
11	29.0	0.02650	1.0	0.00900	0.00500	0.00002	0.00001
12	28.0	0.02890	1.0	0.00900	0.00500	0.00002	0.00001
13	27.0	0.03130	1.0	0.00900	0.00500	0.00002	0.00001
14	26.0	0.03370	1.0	0.00900	0.00500	0.00002	0.00001
15	25.0	0.03620	1.0	0.00900	0.00500	0.00002	0.00001
16	24.0	0.03860	1.0	0.00900	0.00500	0.00002	0.00001
17	23.0	0.04100	1.0	0.00899	0.00500	0.00002	0.00001
18	22.0	0.04340	1.0	0.00893	0.00498	0.00002	0.00001
19	21.0	0.04610	1.0	0.00852	0.00488	0.00002	0.00001
20	20.0	0.05000	1.0	0.00700	0.00450	0.00002	0.00001
21	19.0	0.05610	1.0	0.00548	0.00412	0.00002	0.00001
22	18.0	0.06340	1.0	0.00507	0.00402	0.00002	0.00001
23	17.0	0.07100	1.0	0.00501	0.00400	0.00002	0.00001
24	16.0	0.07860	1.0	0.00500	0.00400	0.00002	0.00001
25	15.0	0.08620	1.0	0.00500	0.00400	0.00002	0.00001
26	14.0	0.09370	1.0	0.00500	0.00400	0.00002	0.00001
27	13.0	0.10133	1.0	0.00500	0.00400	0.00002	0.00001
28	12.0	0.10892	1.0	0.00500	0.00400	0.00002	0.00001
29	11.0	0.11651	1.0	0.00500	0.00400	0.00002	0.00001
30	10.0	0.12410	1.0	0.00500	0.00400	0.00002	0.00001
31	9.0	0.13169	1.0	0.00500	0.00400	0.00002	0.00001
32	8.0	0.13928	1.0	0.00500	0.00400	0.00002	0.00001
33	7.0	0.14687	1.0	0.00500	0.00400	0.00002	0.00001
34	6.0	0.15446	1.0	0.00500	0.00400	0.00002	0.00001
35	5.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
36	4.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
37	3.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
38	2.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
39	1.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001
40	0.0	0.16205	1.0	0.00500	0.00400	0.00002	0.00001

707 The cells below will rerun the end member models for the modified lithospheric  
708 input file. First, equilibrium transport:

```
709 [26]: us_eq = UserCalc.UserCalc(df,stable=False)
df_out_eq = us_eq.solve_all_1D(phi0,n,W0,alpha0_all)
```

710 And second, for disequilibrium transport with  $Da = 0$ :

```
711 [27]: us_diseq = UserCalc.UserCalc(df,model=UserCalc.
↳DisequilTransport, Da=0,stable=False)
df_out_diseq = us_diseq.solve_all_1D(phi0,n,W0,alpha0_all)
```

712 List 6 below displays the activity ratios determined for the final melt compositions  
713 at the end of the two simulations (i.e., the tops of the one-dimensional melting  
714 columns).

```
715 [28]: df_compare = pd.concat([df_out_eq.tail(n=1), df_out_diseq.tail(n=1)])
df_compare['model'] = ['Equilibrium Transport', 'Disequilibrium Transport']
df_compare.set_index('model')
```

```
[28]:
```

	P	z	F	phi	(230Th/238U)
model					
Equilibrium Transport	0.0	0.0	0.16205	0.008	1.015792
Disequilibrium Transport	0.0	0.0	0.16205	0.008	1.039704
		(226Ra/230Th)	(231Pa/235U)	Uf_238U	Uf_230Th
model					
Equilibrium Transport		1.894057	1.792975	-2.901132	-3.473250
Disequilibrium Transport		1.000828	1.034719	-2.891833	-3.440684
	Uf_226Ra	Us_238U	Us_230Th	Us_226Ra	Uf_235U
model					
Equilibrium Transport	-8.355990	-2.901132	-3.473250	-8.355990	-2.902001
Disequilibrium Transport	-8.96132	-30.351986	-30.353121	-30.353146	-2.88492
	Uf_231Pa	Us_235U	Us_231Pa		
model					
Equilibrium Transport	-9.120520	-2.902001	-9.120520		
Disequilibrium Transport	-9.653185	-30.272812	-30.272749		

717 **List 6.** Model output results for the disequilibrium ( $Da = 0$ ) melting scenarios  
718 tested here, with modified lithospheric input conditions.

719 The following cell generates Figure 9, which illustrates outcomes with depth for the  
720 equilibrium and disequilibrium transport models. The model outcomes for the two  
721 transport scenarios are notably different, particularly for the shorter-lived isotopic  
722 pairs.

```
723 [29]: fig, axes = UserCalc.plot_1Dcolumn(df_out_diseq)
axes[2].set_prop_cycle(None)
for s in ['(230Th/238U)', '(226Ra/230Th)', '(231Pa/235U)']:
axes[2].plot(df_out_eq[s],df_out['P'],'--')
```

```
axes[2].set_title('Da = {}'.format(us_diseq.Da))
plt.show()
```

724

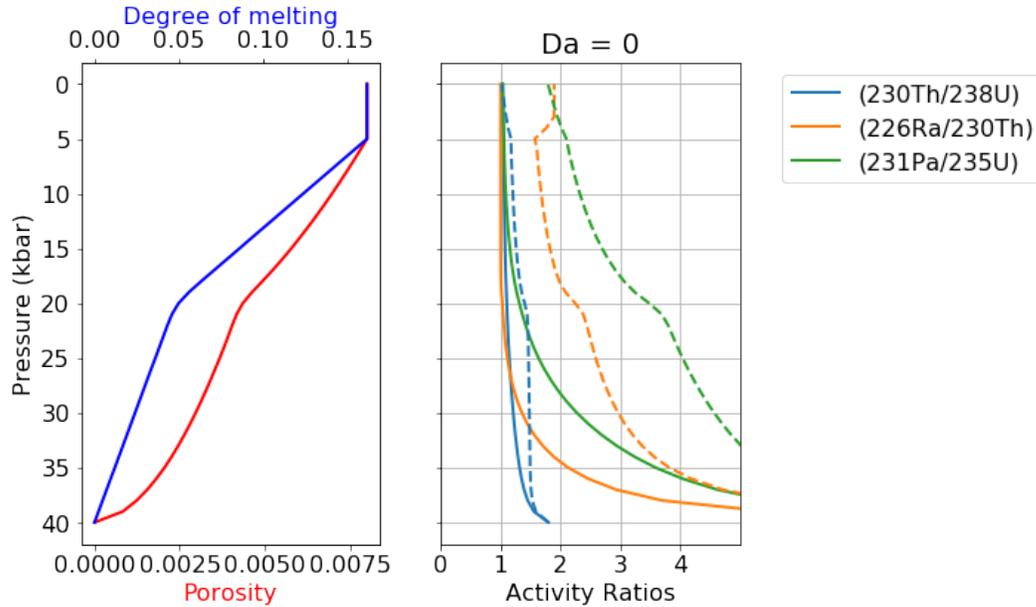


Figure 9: Comparison of equilibrium (dashed) and disequilibrium ( $Da = 0$ ; solid) transport model output results for the degree of melting, residual melt porosity, and activity ratios ( $^{230}\text{Th}/^{238}\text{U}$ ), ( $^{226}\text{Ra}/^{230}\text{Th}$ ), and ( $^{231}\text{Pa}/^{235}\text{U}$ ) as a function of pressure, for the modified lithospheric transport scenario explored above. Symbols and lines as in Figure 3.

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### 3.3 Batch operations

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For many applications, it is preferable to calculate an ensemble of model scenarios over a range of input parameters directly related to questions about the physical constraints on melt generation, such as the maximum residual or reference melt porosity ( $\phi_0$ ) and the solid mantle upwelling rate ( $W_0$ ). The cells below determine a series of one-dimensional column results for the the equilibrium transport model and the parameters defined above (that is, the input conditions shown in Table 3 with  $n = 2$ ,  $\rho_s = 3300 \text{ kg/m}^3$ , and  $\rho_f = 2800 \text{ kg/m}^3$ ), but over a range of values for  $\phi_0$  and  $W_0$ ; these results are then shown in a series of figures. The user can select whether to define the specific  $\phi_0$  and  $W_0$  values as evenly spaced log grid intervals (option 1) or with manually specified values (option 2). As above, all upwelling rates are entered in units of cm/yr. We note that because some of these models tend to be stiff and the Radau solver is relatively computationally expensive, the batch operations below may require a few minutes of computation time for certain scenarios. Here we show the results for the default equilibrium model over a range of selected  $\phi_0$  and  $W_0$  values:

[30]:

```
# Option 1 (evenly spaced log grid intervals):
# phi0 = np.logspace(-3,-2,11)
# W0 = np.logspace(-1,1,11)

# Option 2 (manual selection of values):
```

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```

phi0 = np.array([0.001, 0.002, 0.005, 0.01])
W0 = np.array([0.5, 1., 2., 5., 10., 20., 50.])

import time
tic = time.perf_counter()
toc = time.perf_counter()

# Calculate the U-238 decay chain grid values:
act = us_eq.solve_grid(phi0, n, W0, us_eq.D_238, us_eq.lambdas_238, us_eq.
    ↪ alphas_238)
Th = act[0]
Ra = act[1]
df = pd.DataFrame(Th)
df = pd.DataFrame(Ra)

```

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```

W = 0.5 . . . . .
W = 1.0 . . . . .
W = 2.0 . . . . .
W = 5.0 . . . . .
W = 10.0 . . . . .
W = 20.0 . . . . .
W = 50.0 . . . . .

```

```

[31]: # Calculate the U-235 decay chain grid values:
act_235 = us_eq.solve_grid(phi0, n, W0, us_eq.D_235, us_eq.lambdas_235, ↪
    ↪ us_eq.alphas_235)
Pa = act_235[0]
df = pd.DataFrame(Pa)

```

743

```

W = 0.5 . . . . .
W = 1.0 . . . . .
W = 2.0 . . . . .
W = 5.0 . . . . .
W = 10.0 . . . . .
W = 20.0 . . . . .
W = 50.0 . . . . .

```

744 The figures below illustrate the batch model results in a variety of ways. First, each  
 745 isotopic activity ratio is contoured in  $\phi_0$  vs.  $W_0$  space (Figure 10), using figures sim-  
 746 ilar to the contour plots of Spiegelman (2000). The model outcomes for  $W_0$  and  $\phi_0$   
 747 values are also contoured as mesh "grids" in activity ratio-activity ratio plots (Fig-  
 748 ure 11). These diagrams show the outcomes for model runs with a given  $W_0$  and  $\phi_0$   
 749 value at each grid intersection point, and each curve shows outcomes for a constant  
 750  $W_0$  value with variable  $\phi_0$  or vice versa, as indicated in the figure legend. Because  
 751 this particular example shows results for the equilibrium transport model, and the  
 752 input values for the shallow, spinel peridotite layer of the sample input file define  
 753  $D_U < D_{Th}$ , we note that some of the results exhibit  $(^{230}\text{Th}/^{238}\text{U}) < 1.0$  in Figure 11.

```

[32]: UserCalc.plot_contours(phi0,W0,act, figsize=(12,12))

```

754

```

[33]: UserCalc.plot_contours(phi0,W0,act_235)

```

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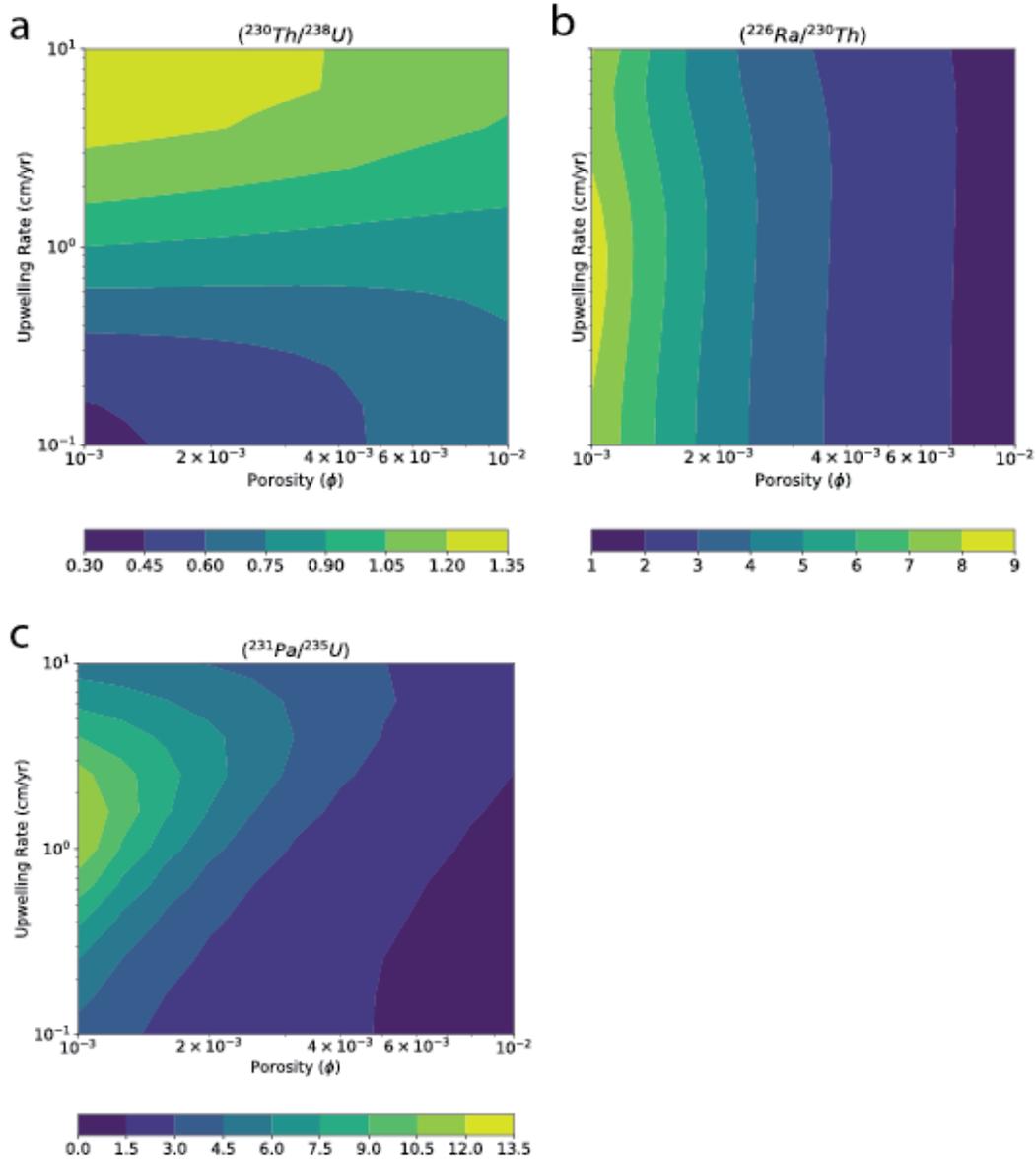


Figure 10: Diagrams of upwelling rate ( $W_0$ ) vs. maximum residual melt porosity ( $\phi$ ) showing contoured activity ratios for (a)  $(^{230}\text{Th}/^{238}\text{U})$ , (b)  $(^{226}\text{Ra}/^{230}\text{Th})$ , and (c)  $(^{231}\text{Pa}/^{235}\text{U})$ .

[34]: `UserCalc.plot_mesh_Ra(Th,Ra,W0,phi0)`

756

[35]: `UserCalc.plot_mesh_Pa(Th,Pa,W0,phi0)`

757

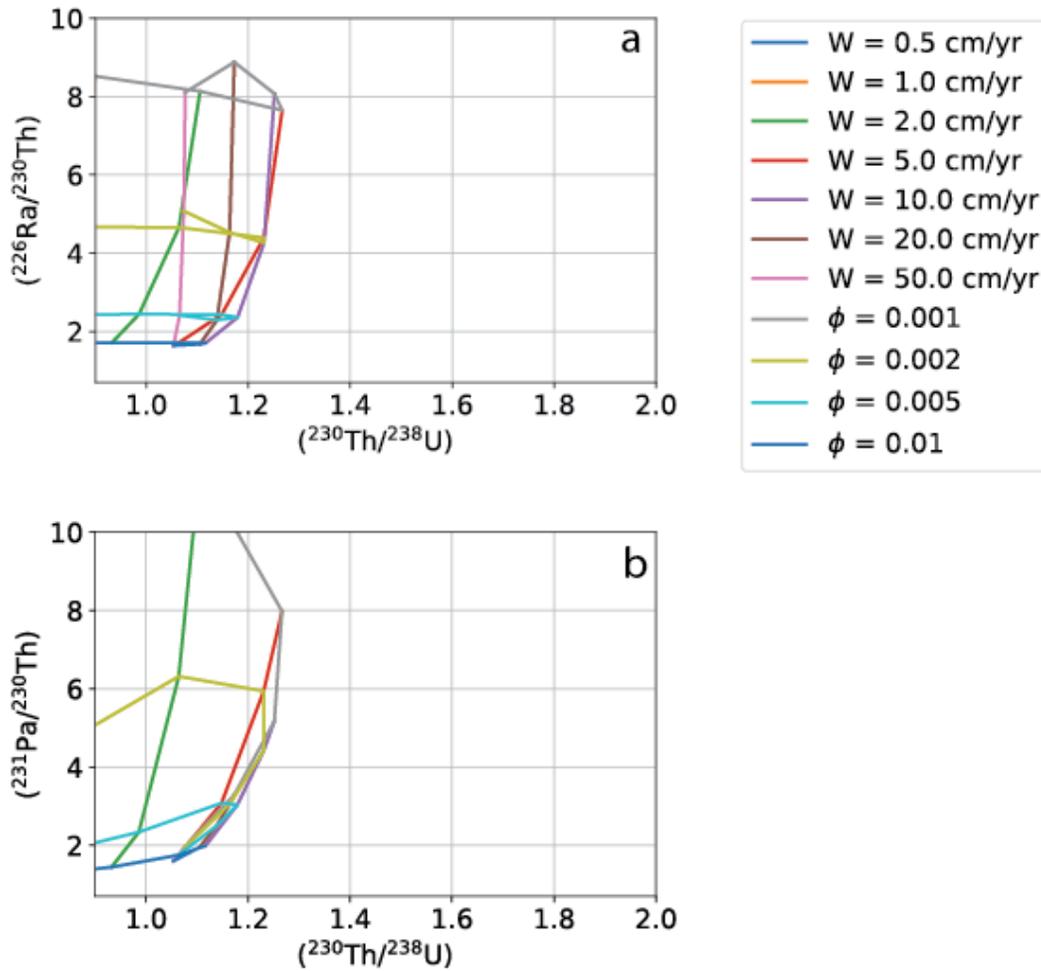


Figure 11: Diagrams showing (a)  $(^{226}\text{Ra}/^{230}\text{Th})$  vs.  $(^{230}\text{Th}/^{238}\text{U})$  and (b)  $(^{231}\text{Pa}/^{230}\text{Th})$  vs.  $(^{230}\text{Th}/^{238}\text{U})$  for the gridded upwelling rate ( $W_0$ ) and maximum residual porosity ( $\phi$ ) values defined above.

#### 4 Summary

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We present pyUserCalc, an expanded, publicly available, open-source version of the UserCalc code for determining U-series disequilibria generated in basalts by one-dimensional, decompression partial melting. The model has been developed from conservation of mass equations with two-phase (solid and liquid) porous flow and permeability governed by Darcy's Law. The model reproduces the functionality of the original UserCalc equilibrium porous flow calculator (Spiegelman, 2000) in pure Python code, and implements a new disequilibrium transport model. The disequilibrium transport code includes reactivity rate-limited chemical equilibration calculations controlled by a Damköhler number,  $Da$ . For stable elements with decay constants equal to zero, the equilibrium model reduces to batch melting and the disequilibrium transport model with  $Da = 0$  to pure fractional melting. The method presented here can be extended to other applications in geochemical porous flow calculations in future work.

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 781 NSF-ACI1550337.

## 782 Data Availability Statement

783 The data set for this research consists of a code package, which  
 784 is available in several ways: 1) in the supporting information, 2)  
 785 through a binder container (at [https://mybinder.org/v2/g1/ENKI-portal%2FpyUsercalc/master?filepath=pyUserCalc\\_manuscript.ipynb](https://mybinder.org/v2/g1/ENKI-portal%2FpyUsercalc/master?filepath=pyUserCalc_manuscript.ipynb)),  
 786 and 3) in the ENKI GitLab data repository (<https://gitlab.com/ENKI-portal/pyUsercalc>), which can also be accessed at the ENKI cloud server  
 787 (<https://server.enki-portal.org/hub/login>) with a free GitLab account (register  
 788 at <https://gitlab.com/ENKI-portal>).

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